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## DIPLOMARBEIT

# Linear stability of the flow in a rectangular 

# cavity driven by oblique lid motion 

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## Declaration of Authorship

I, Johannes Gugler, declare that this thesis titled, "Linear stability of the flow in a rectangular cavity under oblique lid motion" and the work presented in it are my own. I confirm that:

- This work was done wholly or mainly while in candidature for a research degree at this University.
- Where any part of this thesis has previously been submitted for a degree or any other qualification at this University or any other institution, this has been clearly stated.
- Where I have consulted the published work of others, this is always clearly attributed.
- Where I have quoted from the work of others, the source is always given. With the exception of such quotations, this thesis is entirely my own work.
- I have acknowledged all main sources of help.
- Where the thesis is based on work done by myself jointly with others, I have made clear exactly what was done by others and what I have contributed myself.

Signed:

Date:
"When I meet God, I am going to ask him two questions: Why relativity? And why turbulence? I really believe he will have an answer for the first."

Werner Heisenberg

## TU WIEN

Abstract<br>Vienna University of Technology TU Wien<br>Master of Science

## Linear stability of the flow in a rectangular cavity under oblique lid motion

by Johannes Gugler

This thesis is about a linear stability analysis for the lid driven cavity problem. The system of choice consists of a two dimensional rectangular box in $x-$ and $y$-direction, extended to infinity in the 3rd dimension ( $z$-axis). The top lid of the box is moving tangentially to itself with a constant velocity and an inclination angle $\alpha$ with respect to the $x$-axis in the $z$-direction. In this thesis a Python program using the FEniCS library is written to simulate the flow and perform a stability analysis. The lid driven cavity is a benchmark system due to the simple rectangular geometry and therefore much theoretical work has already been done, which allows to test the written code and assure the correctness of the results. A linear stability analysis is carried out and the critical Reynolds numbers are determined as functoins of the cross-sectional aspect ration and the direction of lid motion. The energy budget of critical modes is analyzed using the Reynolds-Orr equation. For some parameter combinations, new modes are found at lower Reynolds numbers than already published results. The correctness of the present results is verified by full 3-dimensional flow simulations.

## Acknowledgements

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## Contents

Declaration of Authorship ..... iii
Abstract ..... vii
Acknowledgements ..... ix
1 Introduction to the problem ..... 1
1.1 The importance of hydrodynamic stability ..... 1
1.2 The lid-driven cavity problem ..... 2
2 Mathematical formulation of the problem ..... 5
2.1 Derivation of the Navier-Stokes equation ..... 5
2.2 Dimensionless formulation of the Navier-Stokes equations ..... 8
2.3 Linear stability ..... 9
2.4 Energy analysis - the Reynolds-Orr equation ..... 11
2.5 Numerical implementation ..... 14
2.5.1 Galerkin methods ..... 14
The finite element method ..... 15
The spectral element method ..... 17
3 Determining the basic flow - convergence studies ..... 19
$3.1 \quad \Gamma=1$ Basic flows ..... 19
3.1.1 Basic flow computed with finite elements ..... 19
Low Reynolds numbers ..... 19
High Reynolds numbers ..... 23
Intermediate Reynolds numbers ..... 24
3.1.2 Comparison with spectral elements ..... 27
Basic flows - comparison with literature ..... 29
$3.2 \quad \Gamma=2$ Basic flows ..... 29
$3.3 \quad \Gamma=3$ Basic flows ..... 30
$3.4 \quad \Gamma=0.5$ basic flows ..... 33
3.5 Conclusion - convergence studies ..... 33
4 Stability analysis ..... 35
4.1 Orthogonal lid motion for $\Gamma=1$ ..... 36
4.2 Stability of oblique cavity flow ..... 36
4.3 Variation of $\Gamma$ between 0.88 and 1.11 ..... 51
$4.4 \quad \Gamma=0.5$ ..... 53
$4.5 \quad \Gamma=2$ ..... 58
$4.6 \quad \Gamma=3$ ..... 63
4.7 Overview of the results of the linear stability analysis ..... 65
5 Summary and Outlook ..... 69
A Derivation of Reynold's transport theorem ..... 71
B Convergence Plots ..... 73
B. $1 \quad \Gamma=1$ ..... 73
B. $2 \Gamma=2$ ..... 80
B.2.1 Re comparison ..... 84
B. $3 \quad \Gamma=3$ ..... 87
B.3.1 Grid convergence studies ..... 87
B.3.2 Re comparison ..... 91
B. $4 \Gamma=0.5$ ..... 94
B.4.1 Grid convergence studies ..... 94
B.4.2 Re comparison ..... 98
C Additional data for Chapter 4 ..... 99
C. 1 Variation of $\Gamma$ ..... 99
C. 2 Critical mode analysis $\Gamma=1, \alpha=7^{\circ}, y=0.2$ ..... 99
D Scripts ..... 107
D. 1 Python - FENICS control ..... 107
D.1.1 Calculation script ..... 107
D.1.2 Plotting script ..... 122
Bibliography ..... 131

## Chapter 1

## Introduction to the problem

This work is concerned with a stability analysis of a famous and simple system in fluid dynamics, the lid-driven cavity. The first chapter is meant as a small general introduction to the topic, while the theoretical framework is postponed to chapter 2. To stress the importance and applications of stability and turbulence in fluids, an introduction to the topic is given in section 1.1. The lid-driven cavity as the test system of this study is presented in section 1.2.

### 1.1 The importance of hydrodynamic stability

If a fluid is flowing at a low speed, quantified by the dimensionless Reynolds number, the behaviour of its flow is determined, once the boundary conditions are given. Increasing the velocity of the fluid may result in multiple solutions of the problem, which tend to preserve the symmetries of the underlying equations and boundary conditions. However, the existence of mulitple solutions may lead to a spontaneous symmetry breaking, which results in a bifurcation to other solutions. In order to be observed in experiment, the mathematical solution of the problem has to be stable, as it would decay otherwise. If the conditions of a basic flow are altered by the application of a disturbance, this disturbance may either decrease or increase in time. If the latter is the case, the underlying basic flow is said to be unstable. Finding the critical point, where the symmetry changes, is the goal of this thesis. An example for such a breaking of symmetry could be the transition from a two-dimensional to a three-dimensional flow. We will find these critical points, by performing a linear stability analysis, which will be introduced in chapter 2 .

Instabilities also pave the way towards turbulences, which are a nuisance from a mathematical point of view because of the chaotic nature of the flow, which forbids to accurately predict the future state thereof, if the initial conditions are not given to infinite precision. The transition towards turbulence is dependent on the particular flow and may be accompanied by a sequence of bifurcations



Figure 1.1: The lid driven cavity. The origin of the coordinate system will be chosen to be the center of the rectangular cross section in the $x-y$ plane.
(for example in a Taylor-Couette or Benard system) or by a complete breaking of all symmetries (for example in a pipe flow). From the point of view of applications turbulences are unwanted when fluids are transported because they are accompanied by the evolution of interacting eddies, which causes drag and thus needs more energy for transport. However, there are cases, where turbulence is helpful in applications, e.g. when fluids are to be mixed. The transition towards turbulence is of utmost importance in understanding the physics of the atmosphere, in aircraft and in industrial applications. The importance of turbulence is reflected by Richard Feynman saying that "Turbulence is the most important unsolved problem of classical physics" ${ }^{1}$.

### 1.2 The lid-driven cavity problem

In this work, we will be concerned with a very simple geometry and study the onset of instability in an infinitely extended (in $z$-direction) rectangular container with width $d$ and height $h$ and an aspect ratio $\Gamma=h / d$, where the top lid is moving at a given velocity $V$ and a drive angle $\alpha$, that measures the inclination in the $x$ - $z$-plane. The cavity with the moving lid is depicted in Figure 1.1. This kind of flow was heavily studied in literature for the case of $\alpha=0$, but for $\alpha \neq 0$ only the standard cavity with $\Gamma=1$ was considered up to now. This thesis is about the expansion of the parameter space, as we will

[^0]vary the angles and the aspect ratios to determine the stability boundary of the basic flow. We will write a program to calculate a basic flow and perform a linear stability analysis by applying a small perturbation to the basic flow. To verify the results, we will be concerned with a comparison to the already published work in chapter 3, where the basic flows are calculated and their properties discussed. Before we deal with the technical implementation of the program, we will derive the mathematical foundation, necessary to tackle the stability problem of the lid driven cavity in chapter 2 , where we will see that the determining parameters of the flow are the aspect ratio $\Gamma$, the drive angle $\alpha$ and the Reynolds number $R e$, which is a dimensionless parameter, given by $R e=V d / \nu$, where $\nu$ is the kinematic viscosity of the fluid inside the cavity.

## Chapter 2

## Mathematical formulation of the problem

This chapter is concerned with the theoretical foundations of the descriptions of fluids, which will be used to model the turbulence in the lid-driven cavity problem. First, a short motivation of the Navier-Stokes equations will be given in section 2.1. The following section 2.2 introduces, how the equations are rewritten in dimensionless notation to extract the physically most relevant figures that describe the fluid. The apparatus of linear stability analysis is presented in section 2.3. Section 2.4 provides a structural quantification of critical modes, based on an energy-analysis, where the Reynolds-Orr equation is derived. The last section 2.5 deals with the numerical implementation of the dimensionless Navier-Stokes equations as implemented in the simulation programs used in this work.

### 2.1 Derivation of the Navier-Stokes equation ${ }^{1}$

To derive the Navier-Stokes equations, which are essentially a reformulation of Newtons second law of motion, a preliminary necessity is to clarify the frame of reference, i.e. the way we observe the flow. There exist two different specifications for describing the behaviour of a flow:

- In the Eulerian specification the flow field is in the center of the description. Each quantity $b$ is represented on a fixed point in space $\vec{x}$.
- In the Lagrangian specification the individual particles are considered. They are labelled according to their position $\vec{X}$ at some fixed time $t_{0}$, which is usually chosen to be $t_{0}=0$.

[^1]These specifications come with two types of time derivatives

$$
\begin{align*}
\frac{\partial b}{\partial t} & =\frac{\partial b(\vec{x}, t)}{\partial t}  \tag{2.1a}\\
\frac{D b}{D t} & =\frac{\partial b(\vec{X}, t)}{\partial t} \tag{2.1b}
\end{align*}
$$

where the first one is in the Eulerian specification and therefore accounts for the change of the quantity $b$ at a certain position $\vec{x}$ in space, whereas the second derivative describes the change of the quantity while following the particle which started at $t_{0}$ at $\vec{X}$ and is therefore called the material derivative. The vector field $\vec{v}(\vec{x}, t)$ allows to obtain the position of a fluid particle by solving the equation

$$
\frac{D \vec{x}}{D t}=\vec{v}(\vec{x}, t)=\left(\begin{array}{l}
u  \tag{2.2}\\
v \\
w
\end{array}\right) .
$$

Following the particle, gives a general relation between the time derivatives in the Lagrangian and Eulerian specifications:

$$
\begin{align*}
\frac{D b}{D t} & =\lim _{\Delta t \rightarrow 0} \frac{b(\vec{x}+\Delta \vec{x}, t+\Delta t)-b(\vec{x}, t)}{\Delta t} \\
& =\lim _{\Delta t \rightarrow 0} \frac{b(\vec{x}+\vec{v} \Delta t, t+\Delta t)-b(\vec{x}, t)}{\Delta t} \\
& =\lim _{\Delta t \rightarrow 0} \frac{b(\vec{x}, t)+\vec{\nabla} b(\vec{x}, t) \vec{v} \Delta t+\frac{\partial b(\vec{x}, t)}{\partial t} \Delta t-b(\vec{x}, t)}{\Delta t}  \tag{2.3}\\
& =(\vec{v} \cdot \vec{\nabla}) b(\vec{x}, t)+\frac{\partial b(\vec{x}, t)}{\partial t} .
\end{align*}
$$

If a calculation of the change of an integral quantity, such as mass, momentum or energy, is required, Reynold's transport theorem, whose derivation is given in Appendix A is used:

$$
\begin{equation*}
\frac{D}{D t} \int_{V} b d V=\int_{V}\left(\frac{\partial b}{\partial t}+\vec{\nabla} \cdot(b \vec{v})\right) d V=\int_{V} \frac{\partial b}{\partial t} d V+\oint b(\vec{v} \cdot \vec{n}) d O \tag{2.4}
\end{equation*}
$$

The conservation of mass leads to the continuity equation

$$
\begin{equation*}
0=\frac{D}{D t} \int_{V} \rho d V=\int_{V}(\frac{\partial \rho}{\partial t}+\vec{\nabla} \underbrace{(\rho \vec{v})}_{\vec{j}}) d V \tag{2.5}
\end{equation*}
$$

and since this holds for any arbitrary volume, the differential form also holds

$$
\begin{equation*}
\frac{\partial \rho}{\partial t}+\vec{\nabla} \cdot \vec{j}=0 \tag{2.6}
\end{equation*}
$$

where $\rho$ is the density and $\vec{j}$ the mass flux density. Newton's second law reads

$$
\begin{equation*}
\frac{D}{D t} \int_{V} \rho \vec{v} d V=\oint_{\partial V} \stackrel{\leftrightarrow}{\sigma} \vec{n} d O+\int_{V} \rho \vec{g} d V \tag{2.7}
\end{equation*}
$$

with $\stackrel{\leftrightarrow}{\sigma}$ being the stress tensor, accounting for forces on the surface and $\rho \vec{g}$ accounting for volume forces (e.g. gravity). Using Gauss' divergence theorem and equation (2.5) this may be rewritten as

$$
\begin{equation*}
\int_{V} \rho \frac{D \vec{v}}{D t} d V=\int_{V}(\vec{\nabla} \stackrel{\leftrightarrow}{\sigma}+\rho \vec{g}) d V \tag{2.8}
\end{equation*}
$$

and since the volume is arbitrary again Newton's second law for infinitesimal quantities, expressed in the index notation (and assuming the Einstein notation for sums), gives

$$
\begin{equation*}
\partial_{t} v_{i}+v_{j} \partial_{j} v_{i}=\frac{1}{\rho} \partial_{j} \sigma_{i j}+g_{i} \tag{2.9}
\end{equation*}
$$

The last ingredient to obtain a closed set of equations for the velocity $\vec{v}$ is a closed expression for $\stackrel{\leftrightarrow}{\sigma}$ :
The easiest approach is to neglect the viscous terms ( $\hat{=}$ off-diagonal terms) in $\stackrel{\leftrightarrow}{\sigma}$, which gives the stress-tensor of a perfect fluid, with the pressure $p$ in the diagonal :

$$
\begin{equation*}
\sigma_{i j}=-p \delta_{i j} \tag{2.10}
\end{equation*}
$$

If a linear dependence of the stress-tensor on the strain-rate tensor $D_{i j} \equiv$ $1 / 2\left(\partial_{i} v_{j}+\partial_{j} v_{i}\right)$ is assumed, one obtains the stress-tensor of a Newtonian fluid

$$
\begin{equation*}
\sigma_{i j}=\left(-p+\bar{\mu} \frac{\partial}{\partial x_{k}} v_{k}\right) \delta_{i j}+2 \mu D_{i j} \tag{2.11}
\end{equation*}
$$

where $\bar{\mu}$ and $\mu$ are two material parameters, known as volume viscosity and shear viscosity, respectively. This expression is used in equation (2.9) to obtain the Navier-Stokes equations:

$$
\begin{equation*}
\rho \frac{D v_{i}}{D t}=-\frac{\partial p}{\partial x_{i}}+\frac{\partial}{\partial x_{i}}\left(\bar{\mu} \frac{\partial}{\partial x_{k}} v_{k}\right)+\frac{\partial}{\partial x_{j}}\left(2 \mu D_{i j}\right)+\rho g_{i} \tag{2.12}
\end{equation*}
$$

If an incompressible fluid ( $\partial_{i} v_{i}=0$ ) with constant material parameters $\rho, \mu$ is assumed ${ }^{2}$, the Navier-Stokes equations simplify drastically, giving

$$
\begin{equation*}
\frac{D v_{i}}{D t}=-\frac{1}{\rho} \frac{\partial p}{\partial x_{i}}+\nu \frac{\partial^{2} v_{i}}{\partial x_{j} \partial x_{j}}+g_{i} \tag{2.13}
\end{equation*}
$$

where the kinematic viscosity $\nu=\mu / \rho$ is introduced. This form of the NavierStokes equations will be used in this work to model the instability in the liddriven cavity problem and in addition the gravitational force $g_{i}$ will be neglected.

### 2.2 Dimensionless formulation of the Navier-Stokes equations

The incompressible Navier-Stokes equations in (2.13) contain many quantities, which come with dimensions. Getting rid of the dimensions by a suitable choice of units allows to extract the physical relevant figures.
The path towards a dimensionless equation is paved by introducing the dimensionless quantities

$$
\begin{array}{rrr}
x=\tilde{x} / \tilde{x}_{r} & t=\tilde{t} / \tilde{t}_{r} & v=\tilde{v} / \tilde{v}_{r} \\
\rho=\tilde{\rho} / \tilde{\rho}_{r} & p=\tilde{p} / \tilde{p}_{r} & \nu=\tilde{\nu} / \tilde{\nu}_{r} . \tag{2.15}
\end{array}
$$

Here all the quantities with a tilde have dimensions and the quantities in the enumerator are the ones that appear in equation 2.13, whereas the denominators are reference values that define a certain scale. The purpose of this procedure is to replace the dimensionful quantities by their dimensionless relatives and to identify the remaining prefactors as the physical relevant parameters, allowing to reduce the parameter space drastically:

$$
\begin{align*}
\frac{\partial \tilde{v}_{i}}{\partial \tilde{t}}+\tilde{v}_{j} \frac{\partial \tilde{v}_{i}}{\partial \tilde{x}_{j}} & =-\frac{1}{\tilde{\rho}} \frac{\partial \tilde{p}}{\partial \tilde{x}_{i}}+\tilde{\nu} \frac{\partial^{2} \tilde{v}_{i}}{\partial \tilde{x}_{j} \partial \tilde{x}_{j}}  \tag{2.16}\\
\Rightarrow \quad \frac{\tilde{v}_{r}}{\tilde{t}_{r}} \frac{\partial v_{i}}{\partial t}+\frac{\tilde{v}_{r}^{2}}{\tilde{x}_{r}} v_{j} \frac{\partial v_{i}}{\partial x_{j}} & =-\frac{\tilde{p}_{r}}{\tilde{\rho}_{r} \tilde{x}_{r}} \frac{1}{\rho} \frac{\partial p}{\partial x_{i}}+\frac{\tilde{\nu}_{r} \tilde{v}_{r}^{2}}{\tilde{x}_{r}^{2}} \nu \frac{\partial^{2} v_{i}}{\partial x_{j} \partial x_{j}} . \tag{2.17}
\end{align*}
$$

For the lid-driven cavity problem, two sets of units are common in literature:

[^2]|  | $\tilde{x}_{r}$ | $\tilde{v}_{r}$ | $\tilde{t}_{r}$ | $\tilde{\rho}_{r}$ | $\tilde{p}_{r}$ | $\tilde{\nu}_{r}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| a) | $d$ | $V$ | $d / V$ | $\rho$ | $\rho V^{2}$ | $\nu$ |
| b$)$ | $d$ | $\nu / d$ | $h^{2} / \nu$ | $\rho$ | $\rho \nu^{2} / d^{2}$ | $\nu$ |

The two formulations use the material parameters of the fluid $\rho$ and $\nu$, which are constant in our formulation, resulting in $\rho=1$ and $\nu=1$. With these formulations the dimensionless Navier-Stokes equations and boundary conditions read:

$$
\begin{array}{ll}
\frac{\partial v_{i}}{\partial t}+v_{j} \frac{\partial v_{i}}{\partial x_{j}}=-\frac{\partial p}{\partial x_{i}}+\frac{1}{R e} \frac{\partial^{2} v_{i}}{\partial x_{j} \partial x_{j}} & V=1 \\
\frac{\partial v_{i}}{\partial t}+v_{j} \frac{\partial v_{i}}{\partial x_{j}}=-\frac{\partial p}{\partial x_{i}}+\frac{\partial^{2} v_{i}}{\partial x_{j} \partial x_{j}} & V=R e \tag{2.18b}
\end{array}
$$

where we introduced the crucial dimensionless paramater $R e=V d / \nu$, the Reynold's number. Taking a look at the equations (2.18a) and (2.18b), one can conlude that flows with similar $R e$ will behave the same, so a huge dimensional parameter space has been reduced to one single variable, which we will have to scan in order to obtain insight in the stability of the lid driven cavity problem. In the formulation of the lid driven cavity problem $V$ denotes the magnitude of the moving lid, which may have nonzero components in $x$ - and $z$ direction. The inclination angle is the second parameter of the given problem. The no-slip no-penetration boundary conditions are applied for the non-moving walls. The third parameter of the given problem is of geometrical origin and is the aspect ratio of the cavity, $\Gamma \equiv h / d$. Note that for unsteady problems, the initial state of the velocity field would have to be given for a solution of the problem. The three parameters will be of big concern in this work and all the various types of cavities may be simulated by looping over these parameters. Here, the formulation in equation (2.18b) will be used, in accordance with Albensoeder, Kuhlmann, and Rath (2001).

### 2.3 Linear Stability Analysis

When we are interested in the stability of a flow, we consider what happens to a solution of the Navier-Stokes equations $\boldsymbol{V}_{0}(\vec{x}, t)=\left(\vec{v}_{0}, p_{0}\right)$, if we apply a small perturbation $\tilde{\boldsymbol{V}}(\vec{x}, t)=(\overrightarrow{\tilde{v}}, \tilde{p})$. We will then analyze, how the resulting flow fields $\boldsymbol{V}_{p}(\vec{x}, t)=\left(\vec{v}_{p}, p_{p}\right)=\boldsymbol{V}+\tilde{\boldsymbol{V}}$ evolve in time. According to Lyapunov, there exist three possibilities that could arise in such a situation ${ }^{3}$ :

[^3]- The system is called Lyapunov stable, if, for every $\epsilon>0$ there exists a $\delta>0$ s.t. if $\|\tilde{\boldsymbol{V}}(0)-\boldsymbol{x}\|<\delta$, then for every $t \geq 0$ we have $\left\|\boldsymbol{V}_{p}(t)-\boldsymbol{x}\right\|<\epsilon$.
- The system is called asymptotically stable if it is Lyapunov stable and there exists $\delta>0$ s.t. if $\|\tilde{\boldsymbol{V}}(0)-\boldsymbol{x}\|<\delta$, then $\lim _{t \rightarrow \infty}\left\|\boldsymbol{V}_{p}(t)-\boldsymbol{x}\right\|=0$.
- The system is called exponentially stable if it is asymptotically stable and there exist $\alpha>0, \beta>0, \delta>0$ s.t. if $\left\|\boldsymbol{V}_{p}(0)-\boldsymbol{V}\right\|<\delta$ then $\left\|\boldsymbol{V}_{p}(t)-\boldsymbol{V}\right\| \leq \alpha\left\|\boldsymbol{V}_{p}(t)-\boldsymbol{V}\right\| e^{-\beta t}$.

In our case, we will start from the stationary quasi two-dimensional state with $\partial v_{0 i} / \partial t=\partial v_{0 i} / \partial z=\partial p_{0} / \partial z=\partial p_{0} / \partial t=0$ for a given Reynolds number, drive angle and aspect ratio. Thus, we solve the stationary equations

$$
\begin{align*}
u_{0} \partial_{x} u_{0}+v_{0} \partial_{y} u_{0} & =-\partial_{x} p_{0}+\left(\partial_{x} \partial_{x}+\partial_{y} \partial_{y}\right) u_{0}  \tag{2.19}\\
u_{0} \partial_{x} v_{0}+v_{0} \partial_{y} v_{0} & =-\partial_{y} p_{0}+\left(\partial_{x} \partial_{x}+\partial_{y} \partial_{y}\right) v_{0}  \tag{2.20}\\
u_{0} \partial_{x} w_{0}+v_{0} \partial_{y} w_{0} & =\left(\partial_{x} \partial_{x}+\partial_{y} \partial_{y}\right) w_{0}  \tag{2.21}\\
\partial_{x} u_{0}+\partial_{y} v_{0} & =0 \tag{2.22}
\end{align*}
$$

subject to the boundary conditions

$$
\begin{array}{lll}
u_{0}=R e \cdot \cos (\alpha), & w_{0}=R e \cdot \sin (\alpha) & \text { at } y=\Gamma / 2 \\
& u_{0}=v_{0}=w_{0}=0 & \text { at } x= \pm 1 / 2 \text { or } y=-\Gamma / 2 \tag{2.24}
\end{array}
$$

where $u_{0}, v_{0}, w_{0}$ denote the $x$-, $y$ - and $z$-component of the velocity vector $\vec{v}_{0}$. Once, equations (2.19) - (2.22) subject to the boundary conditions (2.23) and (2.24) have been solved, we may use the solution as a starting guess for the unsteady flow and insert $\boldsymbol{V}_{p}$ in the full Navier-Stokes equations, resulting in

$$
\begin{equation*}
\partial_{t} \tilde{v}_{i}+v_{0 j} \partial_{j} \tilde{v}_{i}+\tilde{v}_{j} \partial_{j} v_{0 i}+\tilde{v}_{j} \partial_{j} \tilde{v}_{i}=-\partial_{i} \tilde{p}+\partial_{j} \partial_{j} \tilde{v} \tag{2.25}
\end{equation*}
$$

If we assume the perturbation to be small, we may neglect the term $\tilde{v}_{j} \partial_{j} \tilde{v}_{i}$, which is nonlinear in the perturbation and employ the normal mode Ansatz

$$
\begin{equation*}
\tilde{\boldsymbol{V}}=\sum_{k, \omega}\binom{\overrightarrow{\tilde{v}}(x, y)}{\tilde{p}(x, y)} e^{i(k z-\omega t)} e^{-\sigma t} \quad k, \omega, \sigma \in \mathbb{R} \tag{2.26}
\end{equation*}
$$

which is promising due to the homogeneity of the basic flow in $z$-direction. Depending on the sign of $\sigma$, we can deduce, whether a given mode is exponentially
stable or not. If we insert the resulting $\boldsymbol{V}_{p}$ in the Navier-Stokes equations, we arrive at the generalized eigenvalue problem:

$$
\begin{aligned}
& \text { i) } \tilde{u} \partial_{x} u_{0}+\tilde{v} \partial_{y} u_{0}+u_{0} \partial_{x} \tilde{u}+v_{0} \partial_{y} \tilde{u}+w_{0} i k \tilde{u}+\partial_{x} \tilde{p}-\left(\partial_{x} \partial_{x}+\partial_{y} \partial_{y}\right) \tilde{u} \\
& \quad=(\sigma+i \omega) \tilde{u}
\end{aligned}
$$

ii) $\tilde{u} \partial_{x} v_{0}+\tilde{v} \partial_{y} v_{0}+u_{0} \partial_{x} \tilde{v}+v_{0} \partial_{y} \tilde{v}+w_{0} i k \tilde{v}+\partial_{y} \tilde{p}-\left(\partial_{x} \partial_{x}+\partial_{y} \partial_{y}\right) \tilde{v}$

$$
=(\sigma+i \omega) \tilde{v}
$$

$$
\begin{align*}
& \text { iii) } \tilde{u} \partial_{x} w_{0}+\tilde{v} \partial_{y} w_{0}+u_{0} \partial_{x} \tilde{w}+v_{0} \partial_{y} \tilde{w}+w_{0} i k \tilde{w}+i k \tilde{p}-\left(\partial_{x} \partial_{x}+\partial_{y} \partial_{y}\right) \tilde{w}+k^{2} \tilde{w} \\
& \quad=(\sigma+i \omega) \tilde{w} \tag{2.27}
\end{align*}
$$

iv) $\partial_{x} \tilde{u}+\partial_{y} \tilde{v}+i k \tilde{w}=0$
subject to the boundary conditions:

$$
\begin{equation*}
\overrightarrow{\vec{v}}=0 \text { at all boundaries . } \tag{2.28}
\end{equation*}
$$

Solving this generalized eigenvalue problem for different values of $\Gamma, \alpha, R e, k$ allows to investigate the stability for this parameter space. In particular important are the points, where a flow starts to evolve instabilities of the basic flow, which corresponds to negative decay rates $\sigma$. The Reynolds numbers for which $\sigma=0$ are called neutral Reynolds numbers $R e_{n}$. The lowest neutral Reynolds number for a given $\Gamma, \alpha$ is called critical Reynolds number $R e_{c}$. This thesis will be mainly concerned with finding $R e_{n}$ and $R e_{c}$ for a given aspect ratio and drive angle.

### 2.4 Energy analysis - the Reynolds-Orr equation

When the critical modes are calculated, we can also take a look at where the energy that enhances the perturbation comes from. For this reason we consider the change of the mean kinetic energy per unit mass of the perturbation with time ${ }^{4}$

$$
\begin{equation*}
\frac{d E_{k i n}}{d t}=\frac{d}{d t} \int_{V} \frac{\overrightarrow{\tilde{v}}^{2}}{2} d V=\int_{V} \overrightarrow{\tilde{v}} \cdot \frac{d \overrightarrow{\vec{v}}}{d t} d V=\int_{V} \overrightarrow{\tilde{v}} \cdot \frac{\partial \overrightarrow{\tilde{v}}}{\partial t} d V \tag{2.29}
\end{equation*}
$$

where we assumed that the volume $V$ is time independent and we made use of the fact that the nonlinear term with $\overrightarrow{\tilde{v}} \cdot \vec{\nabla} \overrightarrow{\tilde{v}}$ is energy conserving. This term may be rewritten by inserting the linearized Navier-Stokes equations (2.27) to

[^4]give
\[

$$
\begin{equation*}
\frac{d E_{k i n}}{d t}=\int_{V}(\underbrace{-\tilde{v}_{i} \tilde{v}_{j} \partial_{j} v_{0 j}}_{I} \underbrace{-\tilde{v}_{i} v_{0 j} \partial_{j} \tilde{v}_{i}}_{I I} \underbrace{-\tilde{v}_{i} \tilde{v}_{j} \partial_{j} \tilde{v}_{i}}_{I I I} \underbrace{-\tilde{v}_{j} \partial_{i} p}_{I V}+\underbrace{\tilde{v}_{i} \partial_{j} \partial_{j} \tilde{v}_{i}}_{V}) d V \tag{2.30}
\end{equation*}
$$

\]

The terms $I I$ and $I I I$ in this equation vanish because we get the same expressions with a different sign by an integration by parts, using the boundary conditions and the fact that we deal with an incompressible fluid:

$$
\begin{align*}
\int_{V} d V \tilde{v}_{i} v_{0 j} \partial_{j} \tilde{v}_{i} & =\int_{V} d V \partial_{j}\left(\tilde{v}_{i} v_{0 j} \tilde{v}_{i}\right)-\int_{V} d V \tilde{v}_{i}\left(\partial_{j} \tilde{v}_{i} v_{0 j}\right)  \tag{2.31}\\
& =\underbrace{\int_{\partial V} d A_{j}\left(\tilde{v}_{i} v_{0 j} \tilde{v}_{i}\right)}_{=0}-\int_{V} d V \tilde{v}_{i} v_{0 j} \partial_{j} \tilde{v}_{i} \tag{2.32}
\end{align*}
$$

and

$$
\begin{align*}
\int_{V} d V \tilde{v}_{i} \tilde{v}_{j} \partial_{j} \tilde{v}_{i} & =\int_{V} d V \partial_{j}\left(\tilde{v}_{i} \tilde{v}_{j} \tilde{v}_{i}\right)-\int_{V} d V \tilde{v}_{i}\left(\partial_{j} \tilde{v}_{i} \tilde{v}_{j}\right)  \tag{2.33}\\
& =\underbrace{\int_{\partial V} d A_{j}\left(\tilde{v}_{i} \tilde{v}_{j} \tilde{v}_{i}\right)}_{=0}-\int_{V} d V \tilde{v}_{i} \tilde{v}_{j} \partial_{j} \tilde{v}_{i} \tag{2.34}
\end{align*}
$$

The term $I V$ also vanishes due to incompressibility and the boundary conditions for $\tilde{v}$ and term $V$ may be integrated by parts, such that we arrive at the Reynolds-Orr equation:

$$
\begin{equation*}
\frac{d E_{k i n}}{d t}=\int_{V}\left(-\tilde{v}_{i} \tilde{v}_{j} \partial_{j} v_{0 i}-\left(\partial_{j} \tilde{v}_{i}\right)^{2}\right) d V \tag{2.35}
\end{equation*}
$$

The second term in this equation is always negative and called the dissipation rate. The only term which may be responsible for a production of kinetic energy in the perturbation mode is the first term which is called the production rate even though it may also cause energy loss. To understand the mechanism of the local production of kinetic energy it is convenient to split the perturbation in contributions parallel and orthogonal to the basic flow

$$
\begin{equation*}
\overrightarrow{\tilde{v}}_{\|}=\frac{\left(\overrightarrow{\tilde{v}} \cdot \vec{v}_{0}\right) \vec{v}_{0}}{\vec{v}_{0}^{2}} \quad \text { and } \quad \overrightarrow{\tilde{v}}_{\perp}=\overrightarrow{\tilde{v}}-\overrightarrow{\tilde{v}}_{\|} \tag{2.36}
\end{equation*}
$$



Figure 2.1: Energy production rate. a) the gradient of the basic flow is positive and thus the direction of the first and third quadrants are dissipating energy (red regions) and the second and fourth are producing.

This allows to interpret the sign of the production rate, as shown in Figure 2.15. For a comparison with literature, we will decompose the change of the kinetic energy in so called normalized energy transfer terms

$$
\begin{align*}
& D=\frac{1}{D^{*}}\left[\vec{\nabla} \times\left(\overrightarrow{\tilde{v}}_{\perp}+\overrightarrow{\tilde{v}}_{\|}\right)\right]^{2}  \tag{2.37}\\
& I_{1}=-\frac{1}{D^{*}} \overrightarrow{\tilde{v}}_{\perp} \cdot\left(\overrightarrow{\tilde{v}}_{\perp} \cdot \vec{\nabla} \vec{v}_{0}\right)  \tag{2.38}\\
& I_{2}=-\frac{1}{D^{*}} \overrightarrow{\tilde{v}}_{\|} \cdot\left(\overrightarrow{\tilde{v}}_{\perp} \cdot \vec{\nabla} \vec{v}_{0}\right)  \tag{2.39}\\
& I_{3}=-\frac{1}{D^{*}} \overrightarrow{\tilde{v}}_{\perp} \cdot\left(\overrightarrow{\tilde{v}}_{\|} \cdot \vec{\nabla} \vec{v}_{0}\right)  \tag{2.40}\\
& I_{4}=-\frac{1}{D^{*}} \vec{v}_{\|} \cdot\left(\overrightarrow{\tilde{v}}_{\|} \cdot \vec{\nabla} \vec{v}_{0}\right), \tag{2.41}
\end{align*}
$$

where all quantities are normalized by the volume integral of the dissipation rate $D^{*}=\int_{V} D d V$. This decomposition allows to understand the mechanism, which is responsible for the energy production by considering the gradients of the basic flow and the projections on the parallel and orthogonal components of the perturbation. Normalizing the change in kinetic energy, we obtain

$$
\begin{equation*}
\frac{1}{D^{*}} \frac{d E_{k i n}}{d t}=-1+\sum_{i=1}^{4} \int_{V} I_{i} d V \tag{2.42}
\end{equation*}
$$

[^5]which allows for the characterization of a neutral mode, for which the production and dissipation rate are of the same magnitude, s.t. $\sum_{i} \int_{V} I_{i} d V=1$. In this thesis will use the notation $I_{i}$ both for the local as well as the integrated value of each energy contribution. No confusion should arise because the actual meaning is usually deducible from the context. In chapter 4, we will analyze the perturbation modes from the point of view of the Reynolds-Orr equation.

### 2.5 Numerical implementation ${ }^{6}$

In the previous sections, the Navier-Stokes equations were derived and a dimensional analysis for the special case of an incompressible fluid was performed in order to obtain the physical relevant parameters of the problem. This section is concerned with the numerical solution of the problem, where general Galerkin methods are introduced and the specialization of two approaches taken in this work, the finite element and spectral element methods will briefly be explained.

### 2.5.1 Galerkin methods

In this section, we will derive an approach to obtain the solutions of the differential equation

$$
\begin{equation*}
\mathcal{L} f(\vec{x}, t)=0, \tag{2.43}
\end{equation*}
$$

where $\mathcal{L}$ denotes a differential operator. Such a differential equation may be solved numerically by expanding the unknown solution in a set of Ansatz functions ${ }^{7}$

$$
\begin{equation*}
\bar{f}(\vec{x}, t)=\sum_{n=1}^{N} a_{n}(t) \phi_{n}(\vec{x}) \tag{2.44}
\end{equation*}
$$

In this equation the bar above the function $f$ emphazises that the true solution will only be approximated by the finite set of Ansatz functions. The $a_{n}$ are the expansion coefficients and the $\phi_{n}$ denote the Ansatz functions ${ }^{8}$. The insertion of the numerical Ansatz (2.44) in the differential equation (2.43) will not solve

[^6]it exactly but leave some rest $R$, called the residue
\[

$$
\begin{equation*}
\mathcal{L} \bar{f}(\vec{x}, t)=R(\vec{x}, t) . \tag{2.45}
\end{equation*}
$$

\]

Minimization of the residue will give the best agreement between the approximate function $\bar{f}$ and the exact solution $f$. To determine the $a_{n}$, which give the minimal residue, a set of $N$ equations is needed. This set of equations is obtained by weighing the residue with $N$ different weighing functions $W_{m}$ and demanding the weighted residues to be zero

$$
\begin{equation*}
\int_{V} W_{m}(\vec{x}) R(\boldsymbol{x}, t) d V=0, \quad m=1, \ldots, N \tag{2.46}
\end{equation*}
$$

Depending on the choice of the weighing functions, we get different methods for the solution of the differential equation. If the Ansatz functions form an orthogonal basis, a practical choice for the weighing functions $W_{m}$ are the Ansatz functions themselves

$$
\begin{equation*}
W_{m}(\vec{x})=\phi_{m}(\vec{x}) . \tag{2.47}
\end{equation*}
$$

Methods with this choice of weighing functions are called Galerkin methods and will be used in this work.

## The finite element method

In the finite element method the Ansatz functions are chosen to have only finite values at certain regions in space, therefore partitioning the problem in many small ones. In this method, space is partitioned in small divisions, called elements, which supply grid points, called nodes, where the value of the Ansatz function is to be evaluated and supposed to have the same value as the solution function $f(\vec{x}, t)$, s.t. the problem resembles an interpolation of this function in the interstitial region between nodes. The Ansatz functions are chosen to have finite values only in the element, where the node is located and the neighbouring elements. This choice of Ansatz functions will yield block-tridiagonal matrices for the coefficients $a_{n}$ in equation (2.44), when inserted in equation (2.46). The numerical advantage is that block-tridiagonal matrices may be solved very fast by exploiting the sparsity of the matrices. A one-dimensional example would consist of elements, which are represented by lines, and the number of necessary nodes is dependent on the degree of the interpolating Ansatz function, as may be seen in Figure 2.2. For linear interpolation, two nodes per element are
a)

b)


Figure 2.2: a) The structure of a block-tridiagonal matrix, which is easily diagonalized due to its structured sparsity. b)A sketch of two elements in 1d and two linear Ansatz functions $\phi_{j-1}\left(\right.$ red line) and $\phi_{j}$ (blue line). The solution will be exactly represented at the nodes and the functional representation of the solution in element A is given by: $f(x)=a_{j-1} \phi_{j-1}(x)+$

$$
a_{j} \phi_{j}(x) .
$$

sufficient to obtain an accuracy of $\mathcal{O}\left(\Delta x^{2}\right)^{9}$, quadratic interpolation needs three points with an improved accuracy of $\mathcal{O}\left(\Delta x^{3}\right)$. A physicists induction yields that the number of nodes for an interpolation polynomial of order $N$ is $N+1$. The accuracy increases with the order of the interpolation polynomial, however if too many calculations per element have to be performed, it might be advantageous to use a finer mesh and a lower order of interpolation. If convergence is obtained with increasing order of interpolation polynomials the method is called p-FEM, if we converge by increasing the mesh size, we are talking about h-FEM. In this thesis, we will use low order polynomials and check convergence with respect to mesh densities.

For the finite element method we use the code FEniCS (written by Alnæs et al. (2015)), which is a Python/C hybrid, combining the syntax strength of Python with the speed of C , where meshing is already implemented. In the case of the lid-driven cavity, we fill the two-dimensional space with triangular elements. The meshing is already implemented in the program and since the boundaries of the cavity are important to be properly resolved, we use a mesh with a higher

[^7]

Figure 2.3: a) An example for the used meshes for the solution of the Navier-Stokes equations. For illustrational purposes the grid is chosen to be coarse, starting with 20x20 vertex points and after a refinement on the boundary we end up with 576 vertices. b) The Taylor-Hood element: The blue dots denote the nodes for the velocity field and the red dots the ones for pressure.
resolution at the boundaries, as may be seen in Figure 2.3a. Due to convergence reasons we define our functions on a mixed-element space, which is called the Taylor-Hood element. This element implements a quadratic interpolation for the velocity fields, whereas the pressure field is linearly interpolated (see Figure 2.3b). The finite element method will be used in this work for the linear stability study because of the flexibility of the FEniCS program but for comparison, we will also use a different method to crosscheck our results. The workhorse for crosschecking will be the spectral element method.

## The spectral element method

The spectral element method, which we will use to check for convergence with respect to the basis functions, is a hybrid of a spectral method and the finite element method. In the original spectral element methods, the basis functions used in equation (2.44) are usually nonzero over the whole domain and more complex than the simple piecewise polynomials of the FEM, e.g. trigoniometric functions (that is, where the name stems from), Chebyshev polynomials or
high order polynomials. If we merge the local approach from the FEM and use these basis functions inside a given element, we end up with the spectral element method. In general, a more complicated basis function makes the method numerically more time consuming, as the number of evaluation points per element increases. Depending on the basis functions, integrals may be computed faster and more accurately by using special points and weights for their evaluation, similar to Gaussian quadrature. In our case, we can consider the use of the spectral elements as a convergence study with respect to basis functions. Again, we will make use of an already developed open-source code, in this case called NEK5000 (Paul F. Fischer and Kerkemeier (2008)). With these theoretical tools in our hand, we can start to analyze the lid-driven cavities.

## Chapter 3

## Determining the basic flow convergence studies

Before we start to analyze the stability of a given lid-driven cavity, we have to carefully determine the two-dimensional basic flow of the problem. First, we will consider the drive angle $\alpha=0$ in order to compare the flows, obtained with finite elements using FEniCS, with spectral elements using NEK5000 and with lid-driven cavity flows reported in literature. This step is very crucial, because a wrong basic flow will inevitably yield a wrong stability analysis. In this chapter, we will converge the basic flows with respect to mesh sizes, mesh shapes and basis functions. The convergence study will be performed for different Reynolds numbers and aspect ratios $\Gamma$. The plots for $\Gamma \neq 1$ are found in Appendix B.

## $3.1 \quad \Gamma=1$ Basic flows

### 3.1.1 Basic flow computed with finite elements

## Low Reynolds numbers

In order to converge the results more easily, we start our convergence study with low Reynolds numbers. For this purpose, we consider the case $R e=10$. The first simulations are performed on a regular mesh and the Taylor-Hood element ${ }^{1}$. A calculation for a very fine grid with 200 grid points in $x$ - and $y$-direction results in the basic flow shown in Figure 3.1. Since we will want to compare the resulting critical Reynolds numbers with published results, we consider the grid spacing used in the literature to obtain an estimate for the necessary grid density: Albensoeder, Kuhlmann, and Rath (2001) used a finitevolume formulation with a grid of 141 x 141 grid points, but to obtain a finer resolution at the boundaries, they compressed the last 35 cells in each direction

[^8]

Figure 3.1: Basics flow for $R e=10$ : top, The stationary flow for a regular grid with $n_{x}=n_{y}=200$ grid points in each direction. The arrows denote the velocity field and the colour the magnitude of the arrows. The white curves show the streamlines of the flow. bottom, A zoom in the right top edge of the cavity shows the structure of the underlying mesh.


Figure 3.2: Grid comparison $200 \times 200$ versus $250 \times 250$, $R e=10$, the left plot shows the difference in the magnitude of the velocity fields, if the higher resolution grid is interpolated on the coarser grid and the right plot the vice versa interpolation. The lid is located at the top and moves to the right.
by a factor of 0.95 from cell to cell. The second reference (Theofilis, Duck, and Owen 2004) used a spectral method with 128 collocation points.

Our first approach is a regular grid without mesh refinement towards the boundaries. We compare the difference in the resulting magnitude of the velocities and pressures for the case of the highest tractable mesh resolution with $250 \times 250$ grid points ${ }^{2}$. For a graphical comparison, we first use the plotting program VisIt ${ }^{3}$ to interpolate between the mesh points. For a comparison between the data on the two meshes, we can either interpolate the resulting magnitudes of the velocity field from the coarse grid to the fine one or vice versa. Comparing the two variants, we see that the only non-negligible difference of velocity magnitudes is present at the top edges of the cavity (see Figure 3.2). The argument here, however, is to be taken on a qualitative level, because the interpolation from one mesh to the other will give an additional source of error, due to the fact that VisIt does not know about the coefficients of the function in equation (2.44). In addition to this comparison, we calculate the velocities directly in FEniCS along three lines (the two diagonals and the vertical line in the center) using the calculated coefficients for the evaluation of the function values. The results for one diagonal are shown in Figure 3.3, whereas the other two lines are presented in the Appendix (Figure B. 2 and Figure B.3). The convergence studies

[^9]

Figure 3.3: Grid convergence along the diagonal $y=-x+0.5$ from the top left to the right bottom of the cavity. The lines show the interpolated data along the calculated points.
reveal that the edges are the most crucial regions. This is owed to the circumstance that we have a singularity in the boundary conditions at the positions $P_{1}=(-0.5, \Gamma / 2)$ and $P_{2}=(0.5, \Gamma / 2)$. This situation was analyzed by Hancock, Lewis, and Moffatt (1981) and Gupta, Manohar, and Noble (1981), where the streamlines were calculated. There is an interesting feature present in the bottom corners: As Moffatt (1964) has shown, the singular geometry results in progressively weaker counter rotating eddies, which means that the resolution towards the boundary is never able to resolve the correct behavior of the flow in this region. For the case of the stability analysis, we always have to consider this fact and check for the influence of the boundary region on the stability. The difference of the velocities decays very fast towards the center of the cavity, as may be seen in Figure B.1. The conclusion of this is that the mesh resolution is fine in the center of the cavity but needs to be refined towards the boundary. We do this by a refinement procedure, where we first double the mesh resolution for all elements that are less than $30 \%$ of the cavity extensions apart from the borders. The second refinement is done for each element in a vicinity of $15 \%$ and a last refinement for each point within the closest $5 \%$ of the border points. These refinements are done subsequently, such that the mesh density close to the boundary has increased by a factor of 8 . The results of these calculations are visualized in Fig. 3.4 and we see that we can indeed improve convergence in the critical region. The simulations show that a mesh with $60 \times 60$ grid points might be sufficient to obtain proper results. The comparison with VisIt and


Figure 3.4: Grid convergence of the $x$-component of the velocity along the diagonal $y=-x+0.5$ from the top left to the right bottom of the cavity.
the improvement with refinement over the equally spaced grids are shown in the Appendix (Fig. B.4,). Whether the mesh is sufficiently dense will be double checked in the actual calculations of critical $R e-k$ combinations by a subsequent mesh refinement in the vicinity of critical values. Also we will repeat our convergence study for the more interesting cases of higher Re, where critical modes are likely to appear.

## High Reynolds numbers

Since the critical modes arise in a regime of $R e \approx 800$ for the standard cavity with $\Gamma=1$, we will take a look at how the basic flows behave, if the Reynolds numbers are increased. The behaviour of the basic flow with increasing Reynolds numbers is depicted in Appendix B, where a gallery of the basic flows for the Reynolds numbers between 100 and 1000 is given. Since we are only interested in the convergence behaviour with respect to grid size, we will only deal with $R e=800$ here. First, comparing Fig. 3.1 with Fig. 3.5 we see that the relative magnitude of the velocity compared to the lid velocity intrudes deeper into the cavity. Taking a look at the resulting lines with mesh refinement in Fig. 3.6, we can deduce that a $70 \times 70$ mesh looks quite well converged, compared to a $90 \times 90$ mesh, except for the very close vicinity to the boundary. The refinement procedure described in the previous section seems to give a sufficiently converged result also in the case of higher Reynolds numbers. For the stability study, we will therefore start with meshes of $70 \times 70$ to get an estimate for critical


Figure 3.5: $R e=800$ flow. The arrows denote the velocity field and the contour plot its magnitude with the respective legend. The white lines show the streamlines.
wavenumbers, which will be analyzed by a subsequent mesh refinement, to check for convergence of the generalized eigenvalue with mesh size.

## Intermediate Reynolds numbers

The previous calculations have shown, which mesh resolution is necessary in order to obtain an accurate result. Here we will use sufficiently dense meshes to discuss the impact of the Reynolds number on the basic flow for $\Gamma=1$. Increasing the Reynolds number results in a larger vertical penetration depth of the magnitude of the flow velocity inside the cavity, which is shown in Figure 3.7. Comparing the behaviour of the components of the velocity field for different Reynolds numbers along the diagonals of the cavity, we also see that the extrema of $u$ and $v$ shift more towards the boundaries of the cavity, the higher the Reynolds number. The corresponding Figures B. 6 and B. 7 are presented in Appendix B. Up to now, we obtained an estimate for the necessary mesh density within the method of finite elements. In the next sections, we will take a look at the impact of the computational method in use and whether the calculated results are reproducible with another method.


Figure 3.6: Grid convergence. The two plots depict the $x$ - and $y$-components of the velocity field along the line $y=x-0.5$ with refinement towards the boundary.


Figure 3.7: Basic flows. The stationary flows for three Reynolds numbers (A-C) and the comparison between two flows (D, normalized with respect to the lid velocities). In (A-C) the colors denote the magnitude of the velocity field, where red corresponds to big and blue to small values. In (D) red depicts positive and blue negative differences in the velocities, where the maximal relative difference is 0.3649 and the minimal is -0.38 .


Figure 3.8: $R e=10$ differences SEM-FEM. The difference of the magnitude of the velocities on the right top corner of the cavity is shown $\left(\sqrt{\vec{v}_{0}^{S E M} \cdot \vec{v}_{0}^{S E M}}-\sqrt{\vec{v}_{0}^{F E M} \cdot \vec{v}_{0}^{F E M}}\right)$. We see the top right element and 5 Legendre-Gauss-Lobatto points in each direction.

### 3.1.2 Comparison with spectral elements

In order to show the independence of the obtained results on the chosen method, we consider the flows of the previous sections and compare them with results from a spectral element method using the code NEK5000. For the calculations of the flows, we use 9th order polynomials inside the elements on Legendre-Gauss-Lobatto points. The comparison between the flows using a $20 \times 20$ and a $50 \times 50$ element cavity shows, that convergence is obtained for the case of $20 \times 20$ elements. Choosing this resolution, we see that the difference between the finite element approach and the spectral element method is negligible inside the cavity. The biggest difference is visible on the top corners, shown in Fig. 3.8 and may as well be a consequence of the interpolation algorithm used by VisIt similar to the case of in previous section. Also in the case of higher Reynolds numbers, we only encounter a difference in the magnitude of the velocity in the corners of the cavity, as depicted in Figure 3.9.


Figure 3.9: $R e=800$ differences SEM-FEM, The difference of the magnitude of the velocities on the right top corner of the cavity is shown. We see the top right element and 4 Legendre-Gauss-Lobatto points in each direction.


Figure 3.10: Literature comparison $u$ on the vertical center line, the solid green, blue and red line show the calculated component of the $u$ velocity component at the vertical center line. Green crosses mark the minimum of $u$ along the line. The red dots are the results given in Ghia, Ghia, and Shin (1982), the blue horizontal lines mark the minimum of $u$ for $R e=400$ and $R e=1000$ and the blue cross gives the position and minimal value as calculated by Botella and Peyret (1998) and Deng et al.
(1994)

## Basic flows - comparison with literature

To triple-check our results, we compare the calculated flows with some already published results. For the case of $R e=100, R e=400$ and $R e=1000$, Botella and Peyret (1998) and Deng et al. (1994) gave a number of values for the magnitude of the stream function and the vorticity ${ }^{4}$. We will only compare the stream function, since we have chosen a formulation of the equations, where velocity components are most easy to evaluate. The results in Figure 3.10 and Figure 3.11 show that the agreement with previous studies is given to graphical accuracy, because all the literature values lie on the calculated lines.

## $3.2 \quad \Gamma=2$ Basic flows

To shorten the lengthy convergence studies, we will present only the most relevant facts here and the interested reader is provided with additional plots in Appendix B. First, we state that the results of the convergence study show, that

[^10]

Figure 3.11: Literature comparison $v$ on the horizontal center line, the solid green, blue and red line show the calculated component of the $v$ velocity component at the horizontal center line. Green crosses mark the calculated extrema of $v$ along the line. The blue horizontal lines mark the minima and maxima of $v$ for $R e=400$ and $R e=1000$ and the blue crosses give the position and minimal value as calculated by Botella and Peyret (1998) and Deng et al. (1994)
a mesh of $70 \times 70$ grid points before the refinement procedure gives converged results for the velocity components along the diagonals and center lines. The refinement is again performed in a threefold way, s.t. that the points which are $0.6,0.3$ and 0.1 away from the boundary are doubled in the first, second and third refinement, respectively. This shows, that a proper resolution at the boundary allows for a quite coarse grid in the center. With the converged results, we obtain flows for the $\Gamma=2$ case, which are shown in Figure 3.12 and we see that the deeper cavity has enough space to allow for a second counterrotating vortex, whose size and center is dependent on the Re-number and marches towards the boundary for higher Reynolds numbers as the line-plots in Appendix B.2.1 illustrate.

## $3.3 \Gamma=3$ Basic flows

As physicists' induction would suggest, the cavity with an aspect ratio $\Gamma=3$ consists of three vortices, counter-rotating from top to bottom, whose sizes are given by the Reynolds numbers. The flows and the change of the flow pattern with increasing Reynolds number is given in Figure 3.13. The mesh convergence shows, that we need to be careful, when it comes to deeper cavities because a


Figure 3.12: Re comparison for $\Gamma=2$
top left: $R e=100$
top right: $R e=400$
bottom left: $R e=1000$
bottom right: $(R e=100)-(R e=1000)$
The colours denote the magnitude of the velocity and the arrows the direction. The size of the arrows does not represent the magnitude of the velocity but only its direction.


Figure 3.13: $R e$ comparison for $\Gamma=3$
top left: $R e=100$
top right: $R e=400$
bottom left: $R e=1000$
bottom right: $(R e=100)-(R e=1000)$
The colours denote the magnitude of the velocity and the arrows the direction. The size of the arrows does not represent the magnitude of the velocity but only its direction.
mesh of $70 \times 70$ grid points is not converged up to graphical accuracy and may therefore yield wrong results for the stability analysis. When we compare a grid with $70 \times 140$ grid points before refinement, with a $100 \times 100$ grid, we see that convergence is obtained, when the number of grid points in $y$-direction is doubled. The corresponding plots are shown in Appendix B.3.1.

## $3.4 \Gamma=0.5$ basic flows

The last cavity we investigate has an aspect ratio $\Gamma=0.5$. The convergence study in Appendix B.4.1 shows, that a $70 \times 70$ starting mesh results in well converged results, which are in agreement with the spectral element method. This aspect ratio cavity is interesting because of the evolution of a second vortex on the left side of the cavity for higher Reynolds numbers as Figure 3.14 reveals.

### 3.5 Conclusion - convergence studies

The convergence studies have shown that the basic flows are properly resolved by a refinement of the mesh towards the boundary, where a starting mesh of $70 \times 70$ grid points seems to be sufficient to get an estimate for critical Reynolds numbers. Care has to be taken when the aspect ratio is increased above $\Gamma=2$, where a larger number of elements in $y$-direction seems to be appropriate to keep the resolution constant and obtain converged results. We saw that the numerical code developed is able to reproduce published results to graphical precision and can therefore be confident that the basic flows we calculate are correct. For the actual calculations we obtained an impression on how dense the mesh has to be. We will, however, always double check if the obtained result for critical Reynolds numbers and wave vectors is correct, by doing a mesh refinement to investigate the change in the eigenvalues of the generalized eigenvalue equation (2.27).


Figure 3.14: Re comparison for $\Gamma=0.5$
top left: $R e=100$
top right: $R e=400$
bottom left: $R e=1000$
bottom right: $(R e=100)-(R e=1000)$
The colours denote the magnitude of the velocity and the arrows the direction. The size of the arrows does not represent the magnitude of the velocity but only its direction.

## Chapter 4

## Stability analysis

In this chapter, we will use the knowledge of the previous convergence studies and basic flow calculations to disturb the basic flows and obtain the critical modes and Reynolds numbers of the flow. First, we will start to reproduce already published results for $\Gamma=1$ and $\alpha=0$ from Albensoeder, Kuhlmann, and Rath (2001), to check, if the linear stability code works correctly and then we will start to produce new results for different aspect ratios and drive angles. For this purpose a Python class has been developed (the source code is given in Appendix D ), where the necessary functions are implemented to

- find $R e_{c}$ for a given aspect ratio and drive angle by subsequent bisectioning of a given interval of Reynolds numbers. The borders of the input interval $R e_{\text {low }}$ and $R e_{\text {high }}$ should span a region, where critical modes are expected. The resolution of the mesh is adapted, such that we verify the values, where the critical values are arising by a second calculation with a refined mesh (function: findRe_c)
- perform a stability analysis for an array of Reynolds numbers at a given aspect ratio to extract the functional dependence of $\sigma$ on the wavenumber. If a sign change occurs, a subsequent mesh refinement for the wavenumber interval of interest is also implemented in this function (function: analyze).

In order to call these functions in a more user friendly way, a bash script was written, which allows for a hybrid of the previously mentioned functions by a manual change of the wavenumbers of interest in an input file, such that the Python code does not have to be modified for each particular cavity.

These tools allow us to find the critical Reynolds numbers and the values of $k$, where the real part of the growth rate $\sigma$ changes its sign. The size of the parameter space we will investigate in this thesis depends on the computation time of the calculations. If all the calculations converge at the first trial, which is usually not the case, the calculation of 4 angles for a single aspect ratio takes about 3 days on a single core with a very coarse grid in the wavenumber range.

### 4.1 Orthogonal lid motion for $\Gamma=1$

The linear stability analysis of this standard cavity was performed by Albensoeder, Kuhlmann, and Rath (2001), using finite volumes, and by Ding and Kawahara (1999), using finite elements. A comparison between our minimum damping rates $\sigma$ and angular frequencies $\omega$ and theirs are provided in Figure 4.1 and Figure 4.2. The energy transfer rates also agree well with the results obtained in Albensoeder, Kuhlmann, and Rath (2001), both in the magnitude as well as in the localization (see Figure 4.3). The comparison reveals that our code is working well and is able to reproduce published results.

### 4.2 Stability of oblique cavity flow

The flows corresponding to lid motions with inclination angles $\alpha=22.5^{\circ}, 45.0^{\circ}$ and $67.5^{\circ}$ in the $x-z$ plane were analyzed by Theofilis, Duck, and Owen (2004). In their paper, they did not find any critical mode below $R e=800$ for these drive angles, which is in disagreement with this study. As Figure 4.4 reveals, we find critical modes below $R e=800$ for the drive angles $22.5^{\circ}$ and $67.5^{\circ}$. Due to this discrepancy with published results, we also perform an independent three-dimensional non-linear flow simulation of the full Navier-Stokes equation in NEK5000 for the drive angle of $22.5^{\circ}$. From Figure 4.5 we can extract that indeed the velocity at a fixed position starts oscillating ${ }^{2}$. The use of the second method clearly confirms our result by showing that for the $R e=630.7$ flow oscillations arise and grow in time. In addition, the energy analysis suggests, that the production rate exceeds the dissipation rate for the mode of interest, which is another hint for the correctness of the calculation. We also see in Figure 4.4, that the behaviour of the critical parameters follows a non-trivial curve: Increasing the angle from $\alpha=0^{\circ}$ to $\alpha=7^{\circ}$ does not induce a big change in the critical parameters. This plateau is followed by a decrease in $R e_{c}$, which reaches a minimum at an angle of $\alpha \approx 22.5^{\circ}$. The subsequent rise towards a maximal value of $R e_{c} \approx 880$ at an angle of $\alpha=32^{\circ}$ is followed by a decrease towards $R e_{c} \approx 640$ for an angle of $\alpha=55^{\circ}$. There is another plateau between $\alpha=55^{\circ}$ and $\alpha=75^{\circ}$, where there is no rapid change in $R e_{c}$, followed by a small jump at a value of $\alpha=80^{\circ}$.
The limit of an angle of $\alpha=90^{\circ}$ corresponds to a wall bounded Couette flow.

[^11]
(A) $R e=200$

(B) $R e=1000$

Figure 4.1: $\sigma$ comparison with literature, the calculated damping rate $\sigma$ as a function of the wavenumber $k$ is compared with the results of Ding and Kawahara (1999) and Albensoeder, Kuhlmann, and Rath (2001). We see that our calculations are closer to the results of Ding and seem to be converged for a starting mesh of $70 \times 70$ grid points before refinement.


Figure 4.2: $\omega$ comparison with literature. The calculated circular frequency is plotted versus $k$ and compared with Ding and Kawahara (1999) and Albensoeder, Kuhlmann, and Rath (2001) for two different Reynolds numbers. All results agree within a few percent.
$\mathrm{Re}=793.5 \mathrm{k}=15.5177$

(A) Integral energy contributions for the critical mode.

(B) The total energy production rate for the critical mode at $R e_{c}=793.5$ and $k=15.5117$. Shown is the isosurface corresponding to $1 / 5$ of the maximal value. The overall maximum of the energy production is located near the moving lid and the isosurfaces agree with Albensoeder,

Kuhlmann, and Rath (2001).

Figure 4.3: Energy analysis for the critical mode.


Figure 4.4: Critical Reynolds numbers and wavenumbers as a function of $\alpha$ for $\Gamma=1$. The red crosses mark the critical wavenumbers and the blue dots the critical Reynolds numbers.


Figure 4.5: Three-dimensional simulation results with NEK5000 for the drive angle $\alpha=22.5^{\circ}$ with $\Gamma=1$ and $R e=750$. The plot shows the simulation box of the three-dimensional calculations with the lid velocity as an orange arrow. An isosurface of the magnitude of the perturbation velocity is presented. The line plot shows the rising velocity at a fixed position in the cavity and confirms the results obtained with the linear stability analysis. The $x$-axis corresponds to the time and the $y$-axis to the magnitude of the velocity field ${ }^{1}$.

This flow was analyzed by Theofilis, Duck, and Owen (2004), where they did not find any criticality. We also performed a stability analysis for this angle and were likewise unable to find any critical modes for $R e<3000$.
An analysis of all the critical modes for such a large parameter space is impossible and therefore we will focus on the main features apparent, when the angle is varied. Apart from the already clarified discrepancy with Theofilis, Duck, and Owen (2004), there are two interesting jumps occurring in the behaviour of $\operatorname{Re} e_{c}(\alpha)$ for $\Gamma=1$, which shall be analyzed in the following: One jump is occurring in the behaviour of the critical wavenumbers: We see a change in the critical wavenumber arising in the small angle regime: For angles $\alpha<7^{\circ}$, the critical mode is around $k=15$, whereas the spatial periodicity for larger angles is given by wavenumbers with $k_{c}<5$. Taking a look at the $k-\sigma$ curves we realize, that there are two minima of $\sigma$, which are close to criticality and the change of the critical mode is arising between these two angles (Figure 4.6). Since the plot in Figure 4.6 includes points, where the eigenvalue changes rapidly, when $k$ is increased, we will check for this behaviour by a refinement of these critical regions: this is done exemplary for the jump of the second eigenvalue of the $\alpha=7^{\circ}$ case in the regime between $k=9.3$ and $k=9.46$, because we want to


Figure 4.6: $\alpha=6^{\circ}$ and $\alpha=7^{\circ}$, the $k-\sigma$ plots for the analysis of the jump in critical wavenumbers.
see, if our eigenvalue solver is working correctly: We compare the two lowest eigenvalues for eight wavenumbers in this region in Table 4.1 and deduce that the jump is an abrupt change of $\sigma$ with $k$, which means that the eigenvalue solver suddenly finds a new mode. Whether this is of physical origin or owed to the numerics can not be answered at this point.
Due to the fact, that the periodicity of the modes differs a lot, we are also interested in the energy transfer terms and a localization of the energy gain. Figure 4.7 shows the isosurfaces of the production rate in three dimensions. The shapes of the isosurfaces look different: As in the case of $\alpha=0$ in Figure 4.3,

| $k$ | $\sigma_{1}$ | $\sigma_{2}$ | $\omega_{1}$ | $\omega_{2}$ |
| :---: | :---: | :---: | :---: | :---: |
| 9.33 | 50.618 | 139.72 | 2.41 | 232.60 |
| 9.37 | 53.64 | 142.62 | 53.82 | 283.68 |
| 9.39 | 54.40 | 141.93 | 53.18 | 283.07 |
| 9.41 | 55.16 | 141.24 | 52.56 | 280.47 |
| 9.43 | 55.93 | 140.55 | 51.95 | 278.88 |
| 9.44 | 54.81 | 137.04 | 1.24 | 223.67 |
| 9.45 | 55.21 | 136.79 | 1.57 | 222.84 |
| 9.46 | 35.86 | 55.81 | 674.42 | 2.05 |

Table 4.1: Jumps in eigenvalues. The table depicts the behaviour of the eigenvalues for $\alpha=7^{\circ}$ and $R e=784.922$ and corresponds to a section of the turquoise line in Figure 4.6.
there is a banana shaped isosurface at the left side of the cavity. Due to the oblique lid motion these bananas are altered according to the periodicity, given by the wavenumber. The main difference between the two modes are arising in the top right corner. If we take a closer look at the slice $y=0$, as shown in Figure 4.8, we can learn about the mechanism that drives the instability and see the different locations of the production rate between the two modes: The energy production is dominated by the term $I_{2}$. There are two vortices in the surrounding of positive energy production. This may be understood from the energy analysis: Due to the boundary conditions, we have a shear layer with big velocity gradients in $x$-direction and a basic flow in $y$-direction which gives gives a big contribution to $I_{2}$ because the perturbation between the vortices is orthogonal to the basic flow and we see in Figure 4.8 that also the parallel contribution is significant at this location, as the maximal isosurfaces of $v$ are in the vicinity of the maximal production rate. The effect of the different localization on the energy production rate contribution is very small, as depicted in Figure 4.9, which means that the above mentioned mechanism is dominant in both flows. There is only a small shift of weight from $I_{1}$ to $I_{3}$, going from $\alpha=6^{\circ}$ to $\alpha=7^{\circ}$, but the most prominent contribution still comes from $I_{2}$, which resembles the behaviour that was analyzed in Albensoeder, Kuhlmann, and Rath (2001). There is a second interesting slice to look at for the critical mode of $\alpha=7$, which is at an height of $y=0.2$, where the nose shaped feature is located. As we show in Appendix C, this feature stems from the energy transfer rate $I_{3}$.
The second drastic change in the behaviour of the flow is arising between the angles of $\alpha=22.5^{\circ}$ and $\alpha=30^{\circ}$, where $R e_{c}$ is changing from 631 to 862 without a big change in $k_{c}$. As illustrated in Figure 4.10, the energy transfer term distribution is similar for the two observed modes. The critical wavenumber for $\alpha=22.5^{\circ}$ is $k_{c} \approx 7$, whereas the critical mode for $\alpha=30^{\circ}$ is arising at $k \approx 5$ (see Figure 4.11 and Figure 4.12). The spatial localization of the energy gain for the modes is clarified in Figure 4.12. There we show that the energy gain is again along the bananas, as in the case of $\alpha=0^{\circ}$, but at the angle of $\alpha=30^{\circ}$, the energy production at $y=0$ decreases and is shifted to the right side of the cavity (towards $x=0.5$, downstream). Taking a closer look at the slice $y=0$ allows to deduce that the vortex structure of the perturbation changes significantly going from $\alpha=22.5^{\circ}$ to $\alpha=30^{\circ}$. The vortices at $x=-0.5$ vanish for $\alpha=30^{\circ}$. The corresponding Figure 4.13 shows, that the absence of these vortices is accompanied by a reduction of $I_{2}$. This behaviour is explained by a reduced shear as the moving lid induces a flow, whose contribution in $z$-direction


Figure 4.7: Energy productions of the critical modes for $\alpha=6^{\circ}$ (top) and $\alpha=7^{\circ}$ (bottom). An isosurface for a constant value of $\sum_{i} I_{i} / \max \left(\sum_{i} I_{i}\right)$ is shown.


Figure 4.8: Energy productions of the critical modes for $\alpha=6^{\circ}$ (top) and $\alpha=7^{\circ}$ (bottom) at $y=0$. The color denotes the production rate, the arrows denote the $u$ and $w$ components of the velocity and the isolines show the value of $v$, whose extrema are located at the maxima of the production rate.

$$
\begin{array}{rrr}
\Gamma=1.0 \alpha=6.0 & \Gamma=1.0 \alpha=7.0 \\
\operatorname{Re}=799.062 \mathrm{k}=15.0 & \operatorname{Re}=784.922 \mathrm{k}=7.0
\end{array}
$$




Figure 4.9: Energy contributions of the critical modes for $\alpha=6^{\circ}$ (left) and $\alpha=7^{\circ}$ (right).


Figure 4.10: Energy contributions of the critical modes for $\alpha=22.5^{\circ}$ (left) and $\alpha=30.0^{\circ}$ (right)


Figure 4.11: $\sigma$ versus $k$ for $\alpha=22.5^{\circ}$ and $\alpha=30^{\circ}$. We see that the eigenvalues show jumps, where the eigenvalue solver goes to the next eigenvalue, if $k$ is increased. The red line shows, that there is a second mode, where we nearly obtain instability at $k \approx 13$.
increases.
As the shear layer in the $x-y$ plane is diminished are reduced for an angle of $\alpha=30^{\circ}$, we are interested in flows with a very large drive angle. So the next cavity flow we analyze is the one with $\alpha=60^{\circ}$ : The energy contributions show that $I_{2}$ is even more dominant than for smaller angles and the energy production is happening solely in the vicinity of the upstream wall of the cavity, in contrast to the cavity flows analyzed so far.


Figure 4.12: Energy productions of the critical modes for $\alpha=22.5^{\circ}$ with $k=6.83$ (top) and $\alpha=30.0^{\circ}$ with $k=5$ (bottom). An isosurface for a constant value of $\sum_{i} I_{i} / \max \left(\sum_{i} I_{i}\right)=1 / 10$ is shown.


Figure 4.13: Energy productions of the critical modes for $\alpha=22.5^{\circ}$ (top) and $\alpha=30.0^{\circ}$ (bottom) for $y=0.0$. The arrows denote the two-dimensional projection of the perturbation velocity. The colours represent the total local energy production and the isolines $\tilde{v}$.


Figure 4.14: Energy production rate of the critical mode for $\alpha=60^{\circ}$ : The contributions (top left), the sum of the production rates in three dimensions (top right) and on the slice with $y=0.0$ (bottom). The arrows denote the two-dimensional projection of the perturbation velocity. The colours represent the total local energy production and the isolines $\tilde{v}$.

After the detailed analysis of the stability for $\Gamma=1$, we now turn to the parameter dependence of the stability boundary by a variation of $\Gamma$.


Figure 4.15: Variation of $\Gamma$. The critical Reynolds numbers are depicted by circles and the critical $k$ values are plotted as crosses. For the cavity $\alpha=0$ and $\Gamma=0.88$ we see an interesting behaviour, as a new critical mode starts to arise.

### 4.3 Variation of $\Gamma$ between 0.88 and 1.11

Before we start to investigate the criticality in cavities with a completely different aspect ratio, we will vary $\Gamma$ only in a small range around $\Gamma=1$, to investigate the effect of a change in geometry. For this purpose, we consider the same angles as Theofilis, Duck, and Owen (2004), because a denser sampling of $\alpha$ would drastically prolong the computation time. The result of the calculation is shown in Figure 4.15, where we see, that $R e_{c}$ has an interesting behaviour in the $\Gamma, \alpha$ )-plane: For $\alpha=0^{\circ}, \alpha=45^{\circ}$ and $\alpha=67.5^{\circ}, R e_{c}$ decreases for larger aspect ratios and increases for smaller values (with the exception of $\alpha=67.5$ and $\Gamma=1.06$ ). For the case of a drive angle $\alpha=22.5^{\circ}$, a maximum of $R e_{c}$ is found for $\Gamma=1$. The exact quantities are provided in Table C. 1 in Appendix C. The order of $k_{c}$ stays the same over the calculated range of angles, with an interesting exception for the case of $\Gamma=0.88$, where $k_{c}$ of $\alpha=0^{\circ}$ goes down to $k_{c} \approx 6.5$ from a value $k_{c} \approx 16.2$ for $\Gamma=0.90$. This is explained by taking a look at Figure 4.16: At an aspect ratio of $\Gamma=0.88$, the mode at $k \approx 6.5$ starts to govern the criticality of the cavity. Our findings are in agreement with Albensoeder, Kuhlmann, and Rath (2001), where the critical mode for $\Gamma=0.888$ was calculated to be the stationary one we obtain in our regime of aspect ratios for the angle $\alpha=0^{\circ}$. If this oscillatory mode is the critical also for the small


Figure 4.16: $k-\sigma$ for $\Gamma=0.88, \alpha=0.0$ and $\Gamma=0.90, \alpha=0.0$. The first and second eigenvalue of each cavity is shown for the $k$-values of interest. In the lower $k$-regime, the first and second eigenvalues are indistinguishable.
aspect ratio cavities is an interesting question, which we will answer in the next section.

## $4.4 \quad \Gamma=0.5$

The cavity with $\Gamma=0.5$ is of special interest, because the literature shows strong deviations in the arising critical modes: Theofilis, Duck, and Owen (2004) obtained values for 4 neutral modes for the $\alpha=0$ case, where the lowest $R e_{n}$ was calculated to be 1467 for a mode with $k_{c}=13.33$, which is in big contrast with the calculations of Albensoeder, Kuhlmann, and Rath (2001), who obtained the value $R e_{c}=706.1$ for $k_{c}=10.63$. Our first approach did not find the critical mode of Albensoeder, Kuhlmann, and Rath (2001) because our variation steps of $R e$ were too large and we skipped the region of interest, so without the knowledge about the existence of the mode, we would have missed it. This finding creates the need for a very proper search of the Reynolds numbers in order to find the lowest neutral mode.
Taking a look at Figure 4.17, we see that we can reproduce the published results of Albensoeder, Kuhlmann, and Rath (2001). We obtain the criticality for $k_{c}=10.6$ and $R e_{c}=712$, which is a transient mode with $\omega=819$. Thus, the critical mode from the previous section is not responsible for critical one for the aspect ratio of $\Gamma=0.5$. An analysis of the aforementioned mode at $k \approx 6.5$, which was important in the $\Gamma=0.88$ cavity, yields an eigenvalue of $\sigma=97$, far away from being critical. As we have a lot of interesting modes arising for this new geometry, we will not focus on the presence of the $k \approx 6.5$ mode, even though it would be interesting, where the transition from this mode toward ours for $\Gamma=0.5$ occurs. A comparison between Figure 4.17 and Figure 4.4 reveals that the behaviour of the critical Reynolds numbers and wavenumbers with increasing angles shows similarities with the results for $\Gamma=1$, as $k_{c}$ and $R e_{c}$ lower, if we go from $\alpha=0^{\circ}$ to $\alpha=22.5^{\circ}$. The jump of $R e_{c}$ between $\alpha=22.5^{\circ}$ and $\alpha=30^{\circ}$ is also present, whereas the rest of the plot of $\operatorname{Re}_{c}(\alpha)$ does not resemble the $\Gamma=1$ case: First, there is no drop in $R e_{c}$, when the drive angle grows from $\alpha=30^{\circ}$ to $\alpha=60^{\circ}$ and the small enhancement of $R e_{c}$ at $\alpha=67.5^{\circ}$ for $\Gamma=1$ is more pronounced for the geometry with $\Gamma=0.5$. As there are three regions of interest, we will analyze one representative of each:
For the analysis we choose the angles $\alpha=0^{\circ}, \alpha=30^{\circ}$ and $\alpha=67.5^{\circ}$. Comparing the Figures $4.18,4.19$ and 4.20, we learn, that the bigger the angle, the more production rate shifts towards $I_{2}$ and the energy production is more localized. While the lid-driven cavity flow for an angle of $0^{\circ}$ has a contribution $I_{4}$, which accounts for approximately $20 \%$ of the production rate, this value decreases for higher angles, such that $I_{3}$ has a bigger contribution for the $\alpha=30^{\circ}$ flow. The influence of the shear layer on the right side of the cavity ( $x \approx 0.5$, downstream)


Figure 4.17: $\Gamma=0.5-R e_{c}$ and $k_{c}$ versus $\alpha$. The calculated results for the cavities with the given aspect ratio show higher critical Reynolds numbers than the standard cavity with $\Gamma=1$.
is diminished and the vortices in the $x-y$-plane, which are responsible for the energy production mechanism discussed above, vanish for the angle $\alpha=67.5^{\circ}$. The loss of this energy production results in a much higher $R e_{c}$ for the large angle. This completes the treatment of the $\Gamma=0.5$ lid-driven cavity flows and we focus our attention to geometries with bigger aspect ratios and investigate on the stability behaviour also for geometries with $\Gamma>1$.


Figure 4.18: Energy production rate of the critical mode for $\Gamma=0.5$ and $\alpha=0^{\circ}$ : The contributions (top left), the sum of the production rates in three dimensions (top right) and on the slice with $y=0.0$ (bottom). The isosurface for the 3 dimensional plot of the energy production corresponds to the value $\sum_{i} I_{i} / \max \left(\sum_{i} I_{i}\right)=1 / 10$. For the slice at $y=0$ the arrows denote the two-dimensional projection of the perturbation velocity. The colours represent the total local energy production and the isolines $\tilde{v}$.

$$
\begin{array}{r}
\Gamma=0.5 \alpha=30.0 \\
\operatorname{Re}=1112.0 \mathrm{k}=6.5
\end{array}
$$




Figure 4.19: Energy production rate of the critical mode for $\Gamma=0.5$ and $\alpha=30^{\circ}$ : The contributions (top left), the sum of the production rates in three dimensions (top right) and on the slice with $y=0.0$ (bottom). The isosurface for the 3 dimensional plot of the energy production corresponds to the value $\sum_{i} I_{i} / \max \left(\sum_{i} I_{i}\right)=1 / 10$. For the slice at $y=0$ the arrows denote the two-dimensional projection of the perturbation velocity. The colours represent the total local energy production and the isolines $\tilde{v}$.


Figure 4.20: Energy production rate of the critical mode for $\Gamma=0.5$ and $\alpha=67.5^{\circ}$ : The contributions (top left), the sum of the production rates in three dimensions (top right) and on the slice with $y=0.0$ (bottom). The isosurface for the 3 dimensional plot of the energy production corresponds to the value $\sum_{i} I_{i} / \max \left(\sum_{i} I_{i}\right)=1 / 10$. For the slice at $y=0$ the arrows denote the two-dimensional projection of the perturbation velocity. The colours represent the total local energy production and the isolines $\tilde{v}$.


Figure 4.21: $\Gamma=2.0-R e_{c}$ and $k_{c}$ versus $\alpha$. The blue dots denote the critical Reynolds numbers (scale on the left) and the red crosses the critical wavenumbers (scale on the right).

## $4.5 \quad \Gamma=2$

We start the analysis for the lid-driven cavity flow with $\Gamma=2$ by looking at Figure 4.21: First, we notice that the critical Reynolds numbers are lower than for the quadratic cavity with $\Gamma=1$. In contrast to the $\Gamma=0.5$ aspect ratio case, the critical Reynolds numbers decrease, if the drive angles are increased as long as $\alpha<55^{\circ}$. For the largest drive angles analyzed, the critical Reynolds numbers increase, as has been the case for all the aspect ratios we have analyzed up to now. The calculated values for $\alpha=0\left(R e_{c}=458, k_{c}=1.7\right)$ are in good agreement with Albensoeder, Kuhlmann, and Rath (2001) [ $\left.R e_{c}=446.3 \pm 10, k_{c}=1.71\right]$. Again, we take three candidates for a graphical representation of the flow and an analysis of the corresponding energy production mechanism. We consider the angles $\alpha=0^{\circ}, \alpha=45^{\circ}$ and $\alpha=67.5^{\circ}$.

For the angle $\alpha=0$, the analysis is presented in Figure 4.22: The main energy production contribution stems again from $I_{2}$ and the mechanism for energy gain is governed by the existence of two counter-rotating vortices, where the velocity field of the perturbation has the biggest magnitude in the intermediate region. When the fast perturbation reaches the walls, where the shear layer causes a big change of $v_{0}$ with respect to $x$, a negative orthogonal gradient and the parallel $\tilde{v}$ are responsible for a large energy production due to $I_{2}$. This mechanism is the same as in the cavity flow for $\Gamma=1$ and we see that the lower half of the
cavity flow does not give a significant contribution to the energy budget.
The cavity flow for $\alpha=45^{\circ}$ is summarized in Figure 4.23: It has a much lower $R e_{c}=275$ and the vortex structure at $y=0.5$ is removed. The negative energy production at the left (upstream) side of the cavity has diminished in comparison with the flow for the inclination angle $\alpha=0^{\circ}$. The positive and negative extrema of the energy production rates exhibit little spacial separation. The energy production is again strongly correlated with the velocity contribution $\tilde{v}$, orthogonal to the shown plane. The energy contributions $I_{1}, I_{3}$ and $I_{4}$ for the critical mode differ strongly from the $\alpha=0^{\circ}$ critical flow, since most of the weight of $I_{4}$ shifts to $I_{1}$ and $I_{3}$. In contrast to the $\Gamma=0.5$ cavity flows, we do not find the strong decrease of the energy production on the right side (downstream), when the drive angle is increased. This difference in the behaviour of critical flows with increasing angles is manifested when looking at the critical cavity flow for the drive angle $\alpha=67.5^{\circ}$, whose properties are presented in Figure 4.24: We observe, that again the upper vortex (closest to the lid) is mainly responsible for the energy production and that the contribution $I_{2}$ is dominating for large angles, as was the case for all the cavity flows analyzed up to now. The slice at $y=0.5$ reveals another property of the large angle cavity flows for $\Gamma=2$ : While the spots with a positive energy production on the slice located at the vertical center of the upper basic flow vortex have approximately the same size for all the cavity flows, the negative production rate emerges over an increased area, which may explain the higher $R e_{c}$ for the large angle flows.
We saw in this section, that the flows for cavities with an aspect ratio $\Gamma=2$ have a much lower $R e_{c}$ than the smaller aspect ratio flows and that the energy production takes place mainly in the upper half of the cavity. The dependence on the angle turns out to be similar to the $\Gamma=1$ cavity flows, with the difference that the rise of $R e_{c}$ for angles $\alpha<5^{\circ}$ is less pronounced and the lowering of $R e_{c}$ for the angle $\alpha=45^{\circ}$ is $1 / 3$ of $\operatorname{Re}_{c}\left(\alpha=0^{\circ}\right)$. The large angle regime behaviour differs, as there is a continuous rise in $R e_{c}$ as the angle is increased. The curves for $k_{c}$ are similar in the high angle regime, where we obtained a decrease of $k_{c}$ with increasing $\alpha$ for all the aspect ratios.
We continue our analysis by further increasing the aspect ratio and since Figure 4.25 reveals, that the behaviour for $\Gamma=2.5$ resembles the curve of $\Gamma=2$, we will finish our investigations with the cavity flow for an aspect ratio $\Gamma=3$.


Figure 4.22: Energy production rate of the critical mode for $\Gamma=2.0$ and $\alpha=0^{\circ}$ : The contributions (top left), the sum of the production rates in three dimensions (top right) and on the slice with $y=0.5$ (bottom). The isosurface for the 3dimensional plot of the energy production corresponds to the value $\sum_{i} I_{i} / \max \left(\sum_{i} I_{i}\right)=1 / 10$. For the slice at $y=0.5$ the arrows denote the two-dimensional projection of the perturbation velocity. The colours represent the total local energy production and the isolines $\tilde{v}$.

$$
\begin{aligned}
\Gamma & =2.0 \alpha \\
\operatorname{Re} & =275 \mathrm{k}
\end{aligned}=1.8 \mathrm{l} .0 \mathrm{l}
$$



Figure 4.23: Energy production rate of the critical mode for $\Gamma=2.0$ and $\alpha=45^{\circ}$ : The contributions (top left), the sum of the production rates in three dimensions (top right) and on the slice with $y=0.5$ (bottom). The isosurface for the 3 dimensional plot of the energy production corresponds to the value $\sum_{i} I_{i} / \max \left(\sum_{i} I_{i}\right)=1 / 10$. For the slice at $y=0.5$ the arrows denote the two-dimensional projection of the perturbation velocity. The colours represent the total local energy production and the isolines $\tilde{v}$.


Figure 4.24: Energy production rate of the critical mode for $\Gamma=2.0$ and $\alpha=67.5^{\circ}$ : The contributions (top left), the sum of the production rates in three dimensions (top right) and on the slice with $y=0.5$ (bottom). The isosurface for the 3 dimensional plot of the energy production corresponds to the value $\sum_{i} I_{i} / \max \left(\sum_{i} I_{i}\right)=1 / 10$. For the slice at $y=0.5$ the arrows denote the two-dimensional projection of the perturbation velocity. The colours represent the total local energy production and the isolines $\tilde{v}$.


Figure 4.25: $\Gamma=2.5-R e_{c}$ and $k_{c}$ versus $\alpha$. The blue dots denote the critical Reynolds numbers (scale on the left) and the red crosses the critical wavenumbers (scale on the right).

## $4.6 \quad \Gamma=3$

For the aspect ratio $\Gamma=3$, we obtain a higher $R e_{c}=442$ for $\alpha=0$ than Albensoeder, Kuhlmann, and Rath (2001) ( $R e_{c}=424.869$ ) but the trend of decreasing critical Reynolds numbers with increased aspect ratios is continued in accordance with their study. The results differ by $4 \%$, which is not a dramatic difference. This critical perturbation flow is shown in Figure 4.26, where we see that $I_{2}$ is again the biggest energy transfer term and that the energy production is located at the upper basic flow vortex closest to the moving lid. The presented slice at $y=0.75$ on the bottom of Figure 4.26 reveals that the vortex structure of the perturbation in this high energy production surface looks different from the one obtained for the $\Gamma=2$ case in Figure 4.22 as the vortices in the center have vanished. However, this may also be owed to the particular choice of the projection slice at $y=0.75$.
The influence of an increasing drive angle on the critical Reynolds numbers for $\Gamma=3$ cavities was investigated for six angles. The results resemble the behaviour of the $\Gamma=2$ and $\Gamma=2.5$ cavities, with an interesting difference of the critical Reynolds numbers for large angles: As we see in Figure 4.27, there is a very big change in $R e_{c}$ going from $\alpha=50^{\circ}$ to $\alpha=67.5^{\circ}\left(R e_{c}(\alpha=\right.$ $\left.\left.67.5^{\circ}\right)-R e_{c}\left(\alpha=50^{\circ}\right)=666\right)$ and a significant reduction of $R e_{c}$ going from $\alpha=67.5^{\circ}$ to $\alpha=70^{\circ}\left(\operatorname{Re}_{c}\left(\alpha=67.5^{\circ}\right)-\operatorname{Re} e_{c}\left(\alpha=70^{\circ}\right)=181\right)$. A more profound analysis of the critical modes for the critical flows at these two angles is presented


Figure 4.26: Energy production rate of the critical mode for $\Gamma=3.0$ and $\alpha=0.0^{\circ}$. The contributions (top left), the sum of the production rates in three dimensions (top right) and on the slice with $y=0.75$ (bottom). The isosurface for the 3 dimensional plot of the energy production corresponds to the value $\sum_{i} I_{i} / \max \left(\sum_{i} I_{i}\right)=1 / 10$. For the slice at $y=0.75$ the arrows denote the two-dimensional projection of the perturbation velocity. The colours represent the total local energy production and the isolines $\tilde{v}$.


Figure 4.27: $\Gamma=3.0-R e_{c}$ and $k_{c}$ versus $\alpha$. The blue dots denote the critical Reynolds numbers (scale on the left) and the red crosses the critical wavenumbers (scale on the right).
in Figure 4.28 and Figure 4.29, where we extract that they seem to differ only in $R e_{c}$, since the energy production localizations as well as the energy transfer term contributions are similar. Due to this strange behaviour, these calculations were redone with a finer mesh and different parameters for the eigenvalue solver, which did not change the result. If there is physics involved has to be clarified by a three-dimensional simulation, solving the full Navier-Stokes equations.

### 4.7 Overview of the results of the linear stability analysis

We finish our analysis with three-dimensional illustrations of the dependence of the critical values of all the calculated cavity flows on the aspect ratio and drive angle. The results are shown in Figure 4.30. However, it has to be mentioned that some cavity flows were not analyzed as deeply as the ones described above and we may have missed criticality for lower Reynolds numbers, if our $R e$ sampling was not dense enough.


Figure 4.28: Energy production rate of the critical mode for $\Gamma=3.0$ and $\alpha=67.5^{\circ}$ : The contributions (top left), the sum of the production rates in three dimensions (top right) and on the slice with $y=0.75$ (bottom). The isosurface for the 3 dimensional plot of the energy production corresponds to the value $\sum_{i} I_{i} / \max \left(\sum_{i} I_{i}\right)=1 / 10$. For the slice at $y=0.75$ the arrows denote the two-dimensional projection of the perturbation velocity. The colours represent the total local energy production and the isolines $\tilde{v}$.


Figure 4.29: Energy production rate of the critical mode for $\Gamma=3.0$ and $\alpha=70.0^{\circ}$ : The contributions (top left), the sum of the production rates in three dimensions (top right) and on the slice with $y=0.75$ (bottom). The isosurface for the 3 dimensional plot of the energy production corresponds to the value $\sum_{i} I_{i} / \max \left(\sum_{i} I_{i}\right)=1 / 10$. For the slice at $y=0.75$ the arrows denote the two-dimensional projection of the perturbation velocity. The colours represent the total local energy production and the isolines $\tilde{v}$.


Figure 4.30: Results overview. The plots show a threedimensional representation of $R e_{c}$ (top) and $k_{c}$ (bottom) as functions of $\Gamma$ and $\alpha$. The colors of the dots denote the value [bluelow , red-high] and are scaled logarithmically for the upper and linearly for the lower plot.

## Chapter 5

## Summary and Outlook

In this thesis, we introduced the lid-driven cavity problem as an important benchmark system for stability analysis. We presented the mathematical description of the linear stability analysis and the numerical implementation thereof. Subsequently, we developed a code, which is able to accurately determine the properties of the lid driven cavity flows and capable to deal with a change of the geometrical parameter $\Gamma$ and the drive angle $\alpha$ of the moving lid. We showed, that the output of the calculations is comparable with published results for $\alpha=0^{\circ}$ and for the discrepancy with Theofilis, Duck, and Owen (2004) for $\Gamma=1$ and $\alpha=22.5^{\circ}$, we verified our results with a three-dimensional simulation. Thus, we are therefore confident, that the prediction of new critical modes is correct. Whether we always found the lowest Reynolds number, where the transition towards instability occurs can not be guaranteed, because there appeared delicate situations, where our code overlooked modes. This happened, if the criticality of a mode only occurs in a small $R e$ regime, where the search for critical modes by a subsequent bisectioning of the $R e$ interval misses modes, if the guesses for $R e_{c}$ span a big interval.
We found the critical modes, reported in literature and predicted new modes for an expanded parameter space in $\Gamma$ and $\alpha$. For a prediction of the lowest Reynolds numbers, a very profound search was performed to assure that indeed the lowest neutral Reynolds numbers were found. In addition, we were able to analyze the modes of interest with respect to their energy production, both in integral form as well as in local form, where the critical parameters of the flow could be determined and the mechanism that drives the instability could be described. The most prominent mechanism leading to a positive energy production was explained by the effect of a shear layer. For angles $\alpha<45^{\circ}$, counter rotating vortices develop and the intermediate region between the vortices turned out to be the main source for a positive energy production. When the angle was further increased, the vortex structure in the $x-z$ plane was lifted, but the big gradients of the velocities in the shear layer still were the
main sources of positive energy production. The most prominent transfer term was $I_{2}$ for all the analyzed cavity flows.
A further investigation of other neutral modes in the higher Re regime would be of great interest and the change of the critical mode upon a variation of the governing parameters to another might as well be calculated. It would be interesting to see, whether the predicted instabilities can be observed experimentally and in three-dimensional simulations, where the full Navier-Stokes equations are solved. This work provides a search direction for critical modes in such simulations, as guesses for the onset of instability were calculated with the linear stability analysis. This has already enabled us to find new modes, occurring for lower Reynolds numbers as reported by Theofilis, Duck, and Owen (2004).

## Appendix A

## Derivation of Reynold's transport theorem ${ }^{1}$

In this Appendix, Reynold's transport theorem from chapter 2 is derived. As shown there, it is needed to calculate the time derivative in the Lagrangian specification for an integral quantity. For this purpose we need to transform volume elements in the Lagrangian specification (the starting point of the particle is denoted as $\vec{X}=(X, Y, Z)$ to the Eulerian specification (the points in space are denoted as $\vec{x}=(x, y, z)$. This is achieved with the help of the determinant of the Jacobian

$$
\operatorname{det} J=\frac{\partial(x, y, z)}{\partial(X, Y, Z)}=\left|\begin{array}{lll}
\frac{\partial x}{\partial X} & \frac{\partial x}{\partial Y} & \frac{\partial x}{\partial Z}  \tag{A.1}\\
\frac{\partial y}{\partial X} & \frac{\partial y}{\partial Y} & \frac{\partial y}{\partial Z} \\
\frac{\partial z}{\partial X} & \frac{\partial z}{\partial Y} & \frac{\partial z}{\partial Z}
\end{array}\right|,
$$

in index notation $J$ is given by $J_{i j}=\left(\partial x_{i} / \partial X_{j}\right)$. The transformation of the volume element from the Eulerian $(d V)$ to the Lagrangian ( $d V_{0}$ ) specification reads

$$
\begin{equation*}
d V=d V_{0}|\operatorname{det} J| \tag{A.2}
\end{equation*}
$$

This determinant may be calculated by the Laplacian expansion

$$
\begin{equation*}
\operatorname{det} J=\sum_{k=1}^{3} J_{i k} \alpha_{i k} \quad \text { with } \quad \alpha_{i k}=(-1)^{i+k}(\operatorname{det} \tilde{J})_{i k} \text {, } \tag{A.3}
\end{equation*}
$$

where $(\operatorname{det} \tilde{J})_{i k}$ is the minor, which is the subdeterminant resulting by the deletion of the $i$-th row and the $k$-th column. Due to the antisymmetry of the determinant, the following relation holds

$$
\begin{equation*}
\sum_{k=1}^{3} J_{i k} \alpha_{j k}=\delta_{i j} \operatorname{det} J, \tag{A.4}
\end{equation*}
$$

[^12]with $\delta_{i j}$ being the Kronecker-delta. The last needed ingredient for the time derivative of integral quantities, is the material derivative of the Jacobian determinant itself. Starting from the differential of the Laplacian expansion (A.3)
\[

$$
\begin{equation*}
d(\operatorname{det} J)=\sum_{i} \sum_{j} \underbrace{\frac{\partial(\operatorname{det} J)}{\partial J_{i j}}}_{\alpha_{i j}} d J_{i j} \tag{A.5}
\end{equation*}
$$

\]

the material derivative reads

$$
\begin{equation*}
\frac{D(\operatorname{det} J)}{D t}=\sum_{i} \underbrace{\sum_{j} \alpha_{i j}}_{\delta_{k i} d e t J} \frac{D J_{i j}}{D t}=\sum_{i} \sum_{k} \sum_{j} J_{k j} \alpha_{i j} \frac{\partial v_{i}}{\partial x_{k}}=\operatorname{det} J \sum_{i} \underbrace{\frac{\partial v_{i}}{\partial x_{i}}}_{\vec{\nabla} \cdot \vec{v}}, \tag{A.6}
\end{equation*}
$$

where the material derivative of the matrix elements was used

$$
\begin{equation*}
\frac{D J_{i j}}{D t}=\frac{D}{D t}\left(\frac{\partial x_{i}}{\partial X_{j}}\right)=\frac{\partial v_{i}}{\partial X_{j}}=\sum_{k} \frac{\partial v_{i}}{\partial x_{k}} \frac{\partial x_{k}}{\partial X_{j}} . \tag{A.7}
\end{equation*}
$$

Now there is enough equipment to transform the volume integrals and derive Reynold's transport theorem:

$$
\left.\begin{array}{rl}
\frac{D}{D t} \int_{V} b(\vec{x}, t) d V & =\frac{D}{D t} \int_{V_{0}} b(\vec{X}, t) \underbrace{|\operatorname{det} J| d V_{0}}_{d V} \\
& =\int_{V_{0}}(\underbrace{\frac{D|\operatorname{det} J|}{D t}}+|\operatorname{det} J| \frac{D b}{D t} \cdot \vec{v}
\end{array}\right) d V_{0} \quad 1 .
$$

q.e.d.

## Appendix B

## Convergence Plots

This appendix is meant to be a placeholder for the convergence plots, which did not fit in the main text for readability reasons.
B. $1 \quad \Gamma=1$


Figure B.1: The decay of the difference of the velocity magnitude between a $250 \times 250$ grid and a $200 \times 200$ grid from the top left edge ( $x=-0.5, y=0.5$ ) towards the center $(x=0, y=0)$. The parameters of the compared data are $\Gamma=1$ and $R e=10$ and the values on the finer grid were interpolated on the coarser one.


Figure B.2: Grid convergence along the diagonal $y=x-0.5$ from the bottom left to the top right of the cavity. ( $R e=10$, $\Gamma=1$ )


Figure B.3: Grid convergence along a vertical line in the center from the top lid to the bottom. $(R e=10, \Gamma=1)$


Figure B.4: Refined mesh comparison for the velocity field. Top: The difference in magnitude of the velocity between a starting mesh of $160 \times 160$ grid points and $150 \times 150$ grid points, which are refined 3 times as described in the main text.Bottom, The difference divided by the value of the magnitude of the velocity. We see that the maximal difference is about $1 \%$ of the

$$
\text { value. }(R e=10, \Gamma=1)
$$



Figure B.5: $\Gamma=1, R e=800$, grid convergence. The two plots depict the $x$ - and $y$-components of the velocity field along the line $y=x-0.5$ without any refinement towards the boundary.


Figure B.6: $\Gamma=1, u$ along the diagonals of the cavity. The top graph shows $u$ along the diagonal from the top left to the bottom right and the bottom graph depicts the values of $u$ along the other diagonal. We see that the minimum of $u$ shifts towards the boundary with higher Reynolds numbers.


Figure B.7: $\Gamma=1, v$ along the diagonals of the cavity, The top graph shows $v$ along the diagonal from the top left to the bottom right and the bottom graph depicts the values of $v$ along the other diagonal. We see that the minimum of $v$ shifts towards the boundary with higher Reynolds numbers.

## B. $2 \Gamma=2$

This section shows selected plots for the velocity components along the diagonals and center lines of the cavity for $R e=100,400$ and 1000 . The selection is chosen as diverse is possible, s.t. the reader gets an impression for crucial regions and components. From now on we will denote the lines according to their direction, i.e. $\searrow$ and $\swarrow$ for the diagonals and $\downarrow$ and $\rightarrow$ for the two centerlines. We see that a mesh of $70 \times 70$ grid points before the refinement procedure is sufficient to grasp the features of the flow. Convergence up to graphical precision is reached in most of the cases. The only region, where the flows differ slightly is the top left corner but this difference does not have an influence on the flow in the center and may therefore yield good results also for the stability analysis.


Figure B.8: $\Gamma=2, R e=100 u$. The three plots show the $u$-component of the velocity field along the lines $\searrow, \swarrow$ and $\downarrow$, from top to bottom.




Figure B.9: $\Gamma=2, R e=400 v$, the three plots show the $v$ component of the velocity field along the lines $\searrow, \swarrow$ and $\rightarrow$, from top to bottom.




Figure B.10: $\Gamma=2, R e=1000$, the top panel shows the $u$ component along $\searrow$, in the center $v$ along $\searrow$ is shown and on the bottom $v$ along $\swarrow$ is presented.

## B.2.1 Re comparison

This section is meant to illustrate the two effects of an increasing Reynolds number on the flow for the $\Gamma=2$ cavity: The first Figure B. 11 shows that the penetration depth of the magnitude of the velocity increases if the Reynolds number is increased from 100 to 800 and the second Figure B. 12 allows to emphasize the growth of the second vortex with increased $R e$.



Figure B.11: $u$ and $v$ along the diagonal $\searrow$. We see that, as in the case of $\Gamma=1$, the penetration into the cavity is enhanced, if the Reynolds number is increased.


Figure B.12: $u$ and $v$ along the central line $\downarrow$. The second effect of an increased Reynolds number is visible in this plot: the evolution of a second vortex and its growth with higher Reynolds numbers.
B. $3 \Gamma=3$

## B.3.1 Grid convergence studies

This section is a repetition of the previous one for the case of $\Gamma=3$. The convergence studies reveal, that a proper mesh needs at least $70 \times 140$ grid points in order to arrive at results, which are converged up to graphical accuracy.




Figure B.13: $\Gamma=3, R e=100 u$. The three plots show the $u$-component of the velocity field along the lines $\searrow, \swarrow$ and $\downarrow$, from top to bottom.




Figure B.14: $\Gamma=3, R e=400 v$. The three plots show the $v$-component of the velocity field along the lines $\searrow, \swarrow$ and $\rightarrow$, from top to bottom.


Figure B.15: $\Gamma=3, R e=1000$. The top panel shows the $u$ component along $\searrow$, in the center $v$ along $\searrow$ is shown and on the bottom $v$ along $\swarrow$ is presented.

## B.3.2 Re comparison

This section is meant to illustrate the two effects of an increasing Reynolds number on the flow for the $\Gamma=3$ cavity: The first Figure B. 16 indicates the penetration depth of the velocity magnitude with higher Reynolds numbers and the second Figure B. 17 allows to emphasize the growth of the second and third vortices with increased $R e$.


Figure B.16: $u$ and $v$ along the diagonal $\searrow$, we see that, as in the case of $\Gamma=1$, the penetration into the cavity is enhanced, if the Reynolds number is increased.


Figure B.17: $u$ and $v$ along the central line $\downarrow$. The second effect of an increased Reynolds number is visible in this plot: the evolution of a second vortex and its growth with higher Reynolds numbers.

## B. $4 \Gamma=0.5$

## B.4.1 Grid convergence studies

This section provides the convergence studies for $\Gamma=0.5$. It is seen that the quantities are converged for a $70 x 70$ grid. Only small differences are encountered in the very close vicinity of the boundary.


Figure B.18: $\Gamma=0.5, R e=100 u$. The three plots show the $u$-component of the velocity field along the lines $\searrow, \swarrow$ and $\downarrow$, from top to bottom.




Figure B.19: $\Gamma=3, R e=400 v$. The three plots show the $v$-component of the velocity field along the lines $\searrow, \swarrow$ and $\rightarrow$, from top to bottom.




Figure B.20: $\Gamma=3, R e=1000$. The top panel shows the $u$ component along $\searrow$, in the center $v$ along $\searrow$ is shown and on the bottom $v$ along $\swarrow$ is presented.


Figure B.21: $u$ and $v$ along the central line $\rightarrow$.

## B.4.2 Re comparison

In Figure B. 21 we see that for higher $R e$ a second vortex is arising in the $\Gamma=0.5$ cavity.

## Appendix C

## Additional data for Chapter 4

This Appendix holds data and explanations from Chapter 4, which did not fit in the main text.

## C. 1 Table of $R e_{c}$ and $k_{c}$ for the variation of $\Gamma$

## C. 2 Critical mode analysis $\Gamma=1, \alpha=7^{\circ}$

Since there is an interesting feature in the localization of the energy production rate for the critical mode for $\Gamma=1$ and $\alpha=7^{\circ}$, we elaborate on the mechanism of energy production for this mode in this section. The production rate was shown in Figure 4.7, where we explained the mechanism for the main energy gain, stemming from the contribution $I_{2}=-\frac{1}{D^{*}} \overrightarrow{\hat{v}}_{\|} \cdot\left(\overrightarrow{\tilde{v}}_{\perp} \cdot \vec{\nabla} \vec{v}_{0}\right)$. Here, we present the most important contributions for the energy production at the slice with $y=0.2$, where we find an explanation for arising contributions from the term $I_{3}=-\frac{1}{D^{*}} \overrightarrow{\tilde{v}}_{\perp} \cdot\left(\overrightarrow{\tilde{v}_{\|}} \cdot \vec{\nabla} \vec{v}_{0}\right)$. The Figures C.1, C. 2 and C. 3 show the basic flow, the total energy production rate and the separate contributions (the plots are not normalized with $\left.D^{*}\right)$. The Figures illustrate that a big contribution of $I_{2}$ may be seen in this slice with an energy production mechanism that was explained in the main text. However, there are also big regions, where $I_{2}$ is negative and these coincide with the observed nose in the production rate, where the mechanism of energy production is different, as the main contribution at this location comes from $I_{3}$, which means that there has to be a gradient of the basic flow parallel to the velocity field for components which are orthogonal to the flow: The magnitude of the basic flow at the nose position ( $x \approx 0.2$ ) is approximately given by $(+200,-100,+50)$, the perturbation velocity is $\approx(+3,0.1,0)$, resulting in $\overrightarrow{\tilde{v}}_{\|}=(0.84,1.29,-0.54)$ and $\overrightarrow{\tilde{v}}_{\|}=(+3,0.1,0)$. The gradients of the basic flow for $u$ and $v$ are shown in Figure C.4, where we see that the gradients have the form $\nabla v_{i}=(-,+, 0)$ and thus the projection along the parallel perturbation gives a big negative value, which results in a positive production rate, as the contraction

| $\alpha$ | $\Gamma$ | $R e_{c}$ | $k_{c}$ | $\alpha$ | $\Gamma$ | $R e_{c}$ | $k_{c}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 0.000 | 0.880 | 801.172 | 6.538 | 45.000 | 0.880 | 803.613 | 5.789 |
| 0.000 | 0.900 | 810.156 | 16.237 | 45.000 | 0.900 | 795.557 | 5.789 |
| 0.000 | 0.920 | 806.641 | 16.070 | 45.000 | 0.920 | 786.523 | 5.735 |
| 0.000 | 0.940 | 802.734 | 15.819 | 45.000 | 0.940 | 775.781 | 5.682 |
| 0.000 | 0.960 | 798.828 | 15.652 | 45.000 | 0.960 | 764.795 | 5.682 |
| 0.000 | 0.980 | 794.531 | 15.485 | 45.000 | 0.980 | 753.809 | 5.629 |
| 0.000 | 1.000 | 790.312 | 15.266 | 45.000 | 1.000 | 741.875 | 5.621 |
| 0.000 | 1.020 | 785.938 | 15.150 | 45.000 | 1.020 | 730.127 | 5.576 |
| 0.000 | 1.040 | 781.250 | 14.983 | 45.000 | 1.040 | 719.141 | 5.576 |
| 0.000 | 1.060 | 775.781 | 14.816 | 45.000 | 1.060 | 708.887 | 5.576 |
| 0.000 | 1.080 | 770.312 | 14.649 | 45.000 | 1.080 | 699.609 | 5.576 |
| 0.000 | 1.100 | 764.453 | 14.565 | 45.000 | 1.100 | 659.570 | 3.130 |
| 22.500 | 0.880 | 600.391 | 7.350 | 67.500 | 0.880 | 682.031 | 4.101 |
| 22.500 | 0.900 | 608.301 | 7.250 | 67.500 | 0.900 | 676.660 | 4.101 |
| 22.500 | 0.920 | 615.918 | 7.200 | 67.500 | 0.920 | 671.533 | 4.039 |
| 22.500 | 0.940 | 622.070 | 7.150 | 67.500 | 0.940 | 667.139 | 3.977 |
| 22.500 | 0.960 | 627.344 | 7.100 | 67.500 | 0.960 | 663.477 | 3.915 |
| 22.500 | 0.980 | 629.980 | 7.050 | 67.500 | 0.980 | 660.303 | 3.853 |
| 22.500 | 1.000 | 630.703 | 7.035 | 67.500 | 1.000 | 659.688 | 3.775 |
| 22.500 | 1.020 | 628.809 | 6.950 | 67.500 | 1.020 | 656.641 | 3.728 |
| 22.500 | 1.040 | 624.121 | 6.950 | 67.500 | 1.040 | 656.152 | 3.666 |
| 22.500 | 1.060 | 616.211 | 6.850 | 67.500 | 1.060 | 662.744 | 3.542 |
| 22.500 | 1.080 | 605.957 | 6.800 | 67.500 | 1.080 | 637.842 | 1.930 |
| 22.500 | 1.100 | 593.359 | 6.750 | 67.500 | 1.100 | 600.244 | 1.961 |

Table C.1: Variation of $\Gamma$ - calculated values


Figure C.1: Top: the basic flow with arrows for the $u$ - and $v$-components of basic flow and the color denotes the magnitude of the $w$-component. Bottom: $\sum_{i} I_{i}$ for the slice at $y=0.2$ for $\Gamma=1$ and $\alpha=7^{\circ}$ for the critical mode. The color denotes the energy production rate, the arrows the $u$ - and $w$-components of the velocity of the perturbation and the isolines denote the $v$-component of the perturbation.


I2



Figure C.2: Energy transfer terms for $y=0.2$ for the critical mode for $\Gamma=1$ and $\alpha=7^{\circ}$, the colors denote the energy production rate, the arrows the $u$ - and $w$-components of the velocity of the perturbation and the isolines denote the $v$-component of the perturbation. The shown energy transfer terms are $I_{1}$ (top) and $I_{2}$ (bottom).




Figure C.3: Energy transfer terms for $y=0.2$ for the critical mode for $\Gamma=1$ and $\alpha=7^{\circ}$, the colors denote the energy production rate, the arrows the $u$ - and $w$-components of the velocity of the perturbation and the isolines denote the $v$-component of the perturbation. The shown energy transfer terms are $I_{3}$ (top) and $I_{4}$ (bottom).
with the orthogonal perturbation does not result in a sign change. The most general thing to extract here is, that the gradients of the basic flow with respect to the $z$-coordinates vanish, which means that for a fixed magnitude of the perturbation vector, the largest possibility for an energy gain is at positions, where $\tilde{w}=0$, which was the case for the mechanisms described in the main text as well as the mechanism for $I_{3}$.


Figure C.4: Basic flow gradients at $y=0.2, x=0.2$ ( $\Gamma=$ $1, \alpha=7^{\circ}$,top: $u$, bottom: $v$. The background is colored with the magnitude of the velocity component and the arrows denote the respective gradients.

## Appendix D

## Scripts

## D. 1 Python - FENICS control

## D.1.1 Calculation script

```
from fenics import *
import matplotlib
matplotlib.use('pdf')
import matplotlib.pyplot as plt
import scipy.sparse as sp
from scipy.sparse.linalg import eigs
import numpy as np
import os
import sys
class mycav:
    def __init__(self,Gamma, alpha, calcdir=None):
        self.Gamma=Gamma
        self.alpha=alpha
        if (calcdir!=None):
        self.calcdir=calcdir
        if not os.path.exists(calcdir):
        os.mkdir(calcdir)
    def analyze(self,Re,relax_param,lplot=False):
        self.relax_param=relax_param
        print('RUNNING ANALYZE WITH REYNOLDS: {}'.format(Re))
        print('1st RUN }->\mathrm{ coarse GRID')
        filename=self.calcdir+'/'+'Re'+'__{:08.3f}'.format(Re)
        Refile=open(filename,'w')
        karr=np.linspace (0.001,30,30)
        nx=90 #70
        ny=90 #70
        self.getbaseflow(Re, nx, ny)
        sigma,omega=self.linearstab(Re, karr, lplot)
        for line in range(len(sigma)):
            Refile.write('{:10g} {:10g} {:10g} \n'.format(karr[line],sigma[line
            ],omega[line]))
        nr, changearr, indices=self.getsignchange(sigma)
        print('FOUND {} SIGN CHANGES'.format (nr))
        #1 st REFINEMENT OF THE MESH FOR THE CRITICAL k-VALUES
        if (nr>0):
        nx=100 #80
        ny=100 #80
```

```
8
39
40
4 1
42
43
44
    self.getbaseflow(Re,nx,ny)
    for i in indices:
    k1=karr[i]; k2=karr[i+1]
    conv=100
    kdiff=10
    run=0
    found=True
    while(conv>1e-3 and kdiff > 0.1):
        run+=1
        print('LOOKING IN THE VICINITY OF k= {}'.format(k1))
        k_refine=np.linspace (k1, k2,5)
    sigma2,omega2=self.linearstab(Re, k_refine, lplot)
    nr2, changearr2, indices 2=self.getsignchange(sigma2)
    if(nr2==0 and run==1):
        k1=karr [i - 1]
        k2=karr[i+2]
        continue
        if (nr==2 and run>1):
        found=False
        break
    else:
        k1=k_refine[indices2[0]]
        k2=k_refine[indices2[0]+1]
        found=True
    kdiff=abs(k2-k1)
    conv=abs(self.find_nearest(sigma2,0)[1])
    for line in range(len(sigma2)):
        Refile.write('{:10g} {:10g} {:10g} \n'.format(k_refine[line],
            sigma2[line],omega2[line]))
    if found:
        print('SIGMA(k_crit) before 2nd REFINEMENT: {}'.format(sigma2[indices2
            [0]]))
        #EXTRACT THE VALUE CLOSEST TO O
        kchoose=k_refine[self.find_nearest(sigma2,0) [0]]
        #2nd REFINEMENT TO CHECK FOR CONVERGENCE
        nx=110 #90
        ny=110 #90
        self.getbaseflow (Re, nx, ny)
        sigma2,omega2=self.linearstab (Re, np.asarray ([kchoose]), lplot)
        print('SIGMA(k_crit) after 2nd REFINEMENT: {}'.format(sigma2[0]))
        Refile.write('{:10g} {:10g} {:10g} \n'.format(kchoose,sigma2[0],
            omega2[0]))
    else:
    print('WARNING: DID NOT FIND ZERO AFTER 1st REFINEMENT FOR k = {}'.format(
        karr[i]))
Refile.close()
self.plot_k_sigma(Re,filename)
def findRe_c(self, Re_low, Re_high, lplot=False):
resultname=self.calcdir+'/'+'REc_Gamma_{:5.2f}_alpha_{:5.2 f }'.format(self.
    Gamma, self.alpha)
Resultfile=open(resultname, 'w')
karr=np.linspace (0.001, 30,60)
nx=120 #75
ny=120 #75
Rearr=np.array ([Re_low, Re_high])
Remid=(Re_low +Re_high)/2.
while (np.min(abs(Rearr-Remid))>1.):
```

```
    print('RUNNING findRe_c WITH REYNOLDS: {}'.format(Remid))
    filename=self.calcdir+'/'+'Re_crit'+'_{:08.3f}'.format(Remid)
    Refile=open(filename,'w')
    if (Remid<500):
        self.relax_param=0.5
    elif(Remid>=500 and Remid<1200):
        self.relax_param=0.3
    else:
        self.relax_param=0.1
    self.getbaseflow(Remid,nx,ny)
    sigma,omega=self.linearstab(Remid, karr,lplot)
    for line in range(len(sigma)):
        Refile.write('{:10g} {:10g} {:10g} \n'.format(karr[line],sigma[
            line],omega[line]))
    nr,changearr, indices=self.getsignchange(sigma)
    Resultfile.write('{:7.2f} {:2d} \n'.format(Remid,nr))
    print('FOUND {} SIGN CHANGES'.format(nr))
    if (nr>0):
        Rearr[1]=Remid
    elif(nr==0):
        Rearr[0]= Remid
    Remid=(Rearr[0]+Rearr[1]) / 2.
    Refile.close()
Resultfile.close()
def findRe_c_MORE_EV(self,Re_low,Re_high,nr_EV,kmin,kmax,nr_k, lplot=False):
resultname=self.calcdir+'/'+'REc_Gamma_{:5.2f}_alpha_{:5.2 f }'.format(self.
        Gamma, self.alpha)
    Resultfile=open(resultname,'w')
karr=np.linspace(kmin,kmax,nr_k)
nx=120 #75
ny=120 #75
Rearr=np.array ([Re_low, Re_high])
Remid=(Re_low +Re_high)/2.
while (np.min(abs(Rearr-Remid))>0.2):
    print('RUNNING findRe_c WITH REYNOLDS: {}'.format(Remid))
    filename=self.calcdir+'/'+'Re_crit'+'_{:08.3f}'.format(Remid)
    Refile=open(filename, 'w')
    if(Remid<500):
        self.relax_param=0.5
    elif(Remid>=500 and Remid<1200):
        self.relax_param=0.3
    else:
        self.relax_param=0.1
    self.getbaseflow(Remid,nx,ny)
    sigma_low,omega_low,sigma,omega=self.linearstab_MORE_EV(Remid,karr ,nr_EV,
        lplot)
    for line in range(len(sigma)):
        Refile.write('{:10g} {:10g} {:10g} \n'.format(karr[line],sigma_low[
        line],omega_low[line]))
    Refile.write('OTHER EIGENVALS FOR THIS K-VECTOR: \n')
    for ij in range(nr_EV):
        Refile.write('sigma = {} , omega = {} \n'.format(sigma[line,ij],omega[
            line,ij]))
    nr,changearr,indices=self.getsignchange(sigma_low)
    if(len(indices)==0):
        Resultfile.write('{:7.2f} {:2d} \n'.format(Remid,nr))
    else:
```

```
    Resultfile.write('{:7.2f} {:2d} {:10g} \n'.format(Remid, nr, karr[indices
    [0]]))
    print('FOUND {} SIGN CHANGES'.format(nr))
    if(nr>0) :
        Rearr[1]= Remid
    elif(nr==0):
        Rearr[0]=Remid
    Remid=(Rearr[0]+Rearr [1])/2.
    Refile.close()
Resultfile.close()
def singlescan(self, Gammaarr, alphaarr, Rearr, karr, nx, ny):
nx=100 #75
ny=100 #75
for Gamma in Gammaarr:
    for alpha in alphaarr:
        for Re in Rearr:
            resultname='./'+'SCAN_Gamma_{:5.2 f }_alpha_{:5.2 f }'.format(Gamma, alpha)
            print(, ,,
            PARAMETERS
            Gamma = {}
            alpha= {}
            Re= {}
            k= {}
            ,,', format(Gamma, alpha,Re))
            anafile=open(resultname,'a')
        if ( Re< 500) :
                self.relax_param=0.5
            elif(Re>=500 and Remid<1200):
                self.relax_param =0.3
            else:
                    self.relax_param=0.1
            self.getbaseflow (Re, nx, ny)
            sigma,omega=self.linearstab(Re, karr, lplot)
            for line in range(len(sigma)):
                anafile.write('{:10g} {:10g} {:10g} \n'.format(karr[line],sigma
                    [line],omega[line]))
            anafile.close()
def getbaseflow(self, Re, nx, ny):
    parameters["mesh_partitioner"]= 'ParMETIS'
    #parameters["num_threads"] = 1
    #CREATE THE MESH
    self.mesh=RectangleMesh(Point(-1./2., - self.Gamma/2.),Point (1./2., self.Gamma
        /2.),nx,ny)
    #REFINE THE MESH HERE
    self.mymeshrefine()
    #DEFINE TRIAL AND TEST FUNCTIONS
    self.P2 = VectorElement('P',triangle, degree= 2, dim=3)
    self.P1 = FiniteElement('P',
    self.element = MixedElement([self.P2,self.P1])
    self.W= FunctionSpace(self.mesh, self.element)
    self.duvw, self.dp = TestFunctions(self.W)
    self.du,self.dv,self.dw = split(self.duvw)
    #THE FUNCTIONS FOR THE FORMULATION
    uvwp = Function(self.W)
    uvw,p = split(uvwp)
    u,v,w=split(uvw)
```

```
#THE FUNCTIONS FOR THE STEADY STATE SOLUTION
self.uvwp0 = Function(self.W)
self.uvw0,p0 = split(self.uvwp0)
self.u0,self.v0,self.w0 = split(self.uvw0)
Gamma=self.Gamma
tol=1e-14
#DEFINE THE BOUNDARIES
class BoundN(SubDomain):
    def inside(self,x,on_boundary):
    return on_boundary and near(x[1],Gamma/2., tol)
class BoundSEW(SubDomain):
    def inside(self,x,on_boundary):
    return on_boundary and (near(x[1],-Gamma/2., tol) or near(x[0],-1./2., tol)
                or near(x[0],1./2., tol))
self.bcN=BoundN()
self.bcSEW=BoundSEW()
ubcN = DirichletBC(self.W.sub (0), Constant ((Re*np.cos(self.alpha/180.*np.pi)
        ,0.,Re*np.sin(self.alpha/180.*np.pi))), self.bcN)
ubcSEW= DirichletBC(self.W.sub(0), Constant((0., 0., 0.)), self.bcSEW)
bcs=[ubcSEW,ubcN]
###NS-equation
F}=\mathrm{ self.du*u*u.dx (0)*dx+self.du*v*u.dx(1)*dx+inner(grad(self.du),grad (u))*dx
    +self.du*p.dx(0)*dx +\
    self.dv*u*v.dx(0)*dx+self.dv*v*v.dx(1)*dx+inner(grad(self.dv),grad (v))*dx
        +self.dv*p.dx(1)*dx +\
    self.dw*u*w.dx (0)*dx+self.dw*v*w.dx(1)*dx+inner(grad(self.dw),grad (w))*dx
        +\
    self.dp*u.dx(0)*dx+self.dp*v.dx (1)*dx
J=derivative(F,uvwp)
M=u.dx (0)*dx+v.dx (1)*dx
problem = NonlinearVariationalProblem(F, uvwp, bcs, J=J)
solver = AdaptiveNonlinearVariationalSolver (problem,M)
#solver = NonlinearVariationalSolver(problem)
prm = solver.parameters
prm_nonlin=prm["nonlinear_variational_solver"]
prm_nonlin["newton_solver"]["absolute_tolerance"]= 1E-8
prm_nonlin["newton_solver"]["relative_tolerance"]= 1E-8
prm_nonlin["newton_solver"]["relaxation_parameter"]= self.relax_param
if(self.relax_param<0.2):
    prm_nonlin[" newton_solver"][" maximum_iterations"] = 400
else:
    prm_nonlin["newton_solver"]["maximum_iterations"] = 200
prm_nonlin["newton_solver"]["error_on_nonconvergence"]=True
#prm["newton_solver"][" absolute_tolerance"]=1E-8
#prm["newton_solver"]["relative_tolerance"]=1E-8
#prm["newton_solver "]["maximum_iterations"] = 350
#prm["newton_solver "][" relaxation_parameter"]=relax_param
#prm["newton_solver"]["error_on_nonconvergence"]=False
solver_tolerance=1E-8
solved=False
while not solved:
    if(prm_nonlin["newton_solver"]["relaxation_parameter"]<0.05):
        print( , , ,
        DID NOT CONVERGE !
        PARAMETERS:
        Re: :{:08.4f}
```

```
    Gamma : {:08.4f}
    alpha: : {:08.4f}
    ,',.format(Re, self.Gamma, self.alpha))
        sys.exit()
    uvwp.assign(self.uvwp0)
    try:
        solver.solve(solver_tolerance)
    except:
    prm_nonlin["newton_solver"]["relaxation_parameter"]*=0.8
    self.relax_param*=0.8
    s = ">>> WARNING: newton relaxation parameter lowered to %g <<<"
    print(s % prm_nonlin["newton_solver"]["relaxation_parameter"])
    continue
solved=True
self.uvwp0.assign (uvwp)
return
def linearstab(self, Re, karr, lplot=False):
#THE PERTURBATION-FUNCTIONS
uvwp_p = TrialFunction(self.W)
uvec_p,p_p = split(uvwp_p)
u_p,v_p,w_p = split(uvec_p)
#THE BOUNDARY CONDITIONS FOR THE PERTURBATION
ubcN_p = DirichletBC(self.W.sub(0), Constant ((0., 0., 0.) ), self.bcN)
ubcSEW_p= DirichletBC(self.W.sub(0), Constant((0.,0.,0.)), self.bcSEW)
bcs_p=[ubcSEW_p,ubcN_p]
k=Constant (0.1)
sigma=np.zeros(np.size(karr))
omega=np.zeros(np.size(karr))
for i,ck in enumerate(karr):
    k.assign(ck)
    Fp_real=\
        self.du*self.u0*u_p.dx(0)*dx+self.du*self.v0*u_p.dx(1)*dx+self.du*u_p*
        self.u0.dx(0)*dx+self.du*v_p*self.u0.dx(1)*dx+\
        self.du*p_p.dx(0)*dx+self.du.dx(0)*u_p.dx(0)*dx+self.du.dx(1)*u_p.dx(1)*
            dx+self.du*k**2.*u_p*dx+\
        self.dv*self.u0*v_p.dx(0)*dx+self.dv*self.v0*v_p.dx(1)*dx+self.dv*u_p*
            self.v0.dx(0)*dx+self.dv*v_p*self.v0.dx(1)*dx+
        self.dv*p_p.dx(1)*dx+self.dv.dx(0)*v_p.dx(0)*dx+self.dv.dx(1)*v_p.dx(1)*
            dx+self.dv*k**2.*v_p*dx+\
        self.dw*self.u0*w_p.dx(0)*dx+self.dw*self.v0*w_p.dx(1)*dx+self.dw*u_p*
            self.w0.dx(0)*dx+self.dw*v_p*self.w0.dx(1)*dx+\
        self.dw.dx(0)*w_p.dx (0)*dx+self.dw.dx(1)*w_p.dx (1)*dx+self.dw*k**2.*w_p*
            dx+
        self.dp*u_p.dx(0)*dx+self.dp*v_p.dx(1)*dx
    #
    #
    #
    Fp_imag=
                self.du*self.w0*k*u_p*dx+self.dv*self.w0*k*v_p*dx+self.dw*self.w0*k*
                    w_p*dx+self.dw*k*p_p*dx+self.dp*k*w_p*dx
    B_MAT = \
        self.du*u_p*dx+self.dv*v_p*dx+self.dw*w_p*dx
    #
    Ar = PETScMatrix()
    assemble(Fp_real, tensor=Ar)
    [bc.apply(Ar) for bc in bcs_p]
```

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Ai = PETScMatrix()

```
Ai = PETScMatrix()
assemble(Fp_imag, tensor=Ai)
assemble(Fp_imag, tensor=Ai)
[bc.apply(Ai) for bc in bcs_p]
[bc.apply(Ai) for bc in bcs_p]
M = PETScMatrix()
M = PETScMatrix()
assemble(B_MAT, tensor=M)
assemble(B_MAT, tensor=M)
#\bc.apply(M) for bc in bcs_p]
#\bc.apply(M) for bc in bcs_p]
#
#
bcinds = []
bcinds = []
for bc in bcs_p:
for bc in bcs_p:
    bcdict = bc.get_boundary_values()
    bcdict = bc.get_boundary_values()
    bcinds.extend(bcdict.keys())
    bcinds.extend(bcdict.keys())
# This just converts PETSc to CSR
# This just converts PETSc to CSR
Ar = sp.csr_matrix(Ar.mat().getValuesCSR () [:: - 1])
Ar = sp.csr_matrix(Ar.mat().getValuesCSR () [:: - 1])
Ai = sp.csr_matrix(Ai.mat().getValuesCSR()[::-1])
Ai = sp.csr_matrix(Ai.mat().getValuesCSR()[::-1])
M= sp.csr_matrix(M.mat().getValuesCSR()[::-1])
M= sp.csr_matrix(M.mat().getValuesCSR()[::-1])
# Create shift matrix
# Create shift matrix
#shift = 1.2345e10*np.ones(len(bcinds))
#shift = 1.2345e10*np.ones(len(bcinds))
#S = sp.csr_matrix((shift, (bcinds, bcinds)), shape=Ar.shape)
#S = sp.csr_matrix((shift, (bcinds, bcinds)), shape=Ar.shape)
v, V = eigs(Ar+1.j*Ai, 10, M, sigma=-1.)
v, V = eigs(Ar+1.j*Ai, 10, M, sigma=-1.)
sigma[i],omega[i]=np.sort(v)[0].real, np.sort(v)[0].imag
sigma[i],omega[i]=np.sort(v)[0].real, np.sort(v)[0].imag
print('Re= {}, k = {} lowest_sigma = {}, omega = {}'.format(Re,ck, sigma[i],
print('Re= {}, k = {} lowest_sigma = {}, omega = {}'.format(Re,ck, sigma[i],
    omega[i]))
    omega[i]))
##SAVE THE RESULTING FLOW FUNCTIONS
##SAVE THE RESULTING FLOW FUNCTIONS
egv = Function(self.W)
egv = Function(self.W)
egv_dz = Function(self.W)
egv_dz = Function(self.W)
##index of lowest sigma
##index of lowest sigma
indx = np.argmin(v)
indx = np.argmin(v)
#STORE REAL AND IMAGINARY PART OF THE EIGENVECTOR
#STORE REAL AND IMAGINARY PART OF THE EIGENVECTOR
intsteps=100
intsteps=100
zarr = np.linspace(0., 2.*np.pi/ck, intsteps)
zarr = np.linspace(0., 2.*np.pi/ck, intsteps)
delta_z = zarr[1]-zarr[0]
delta_z = zarr[1]-zarr[0]
D_int=0.
D_int=0.
I1_int=0.
I1_int=0.
I2_int=0.
I2_int=0.
I3_int=0.
I3_int=0.
I4_int=0.
I4_int=0.
Isum_int=0.
Isum_int=0.
Imax = -1.e99
Imax = -1.e99
iwhere=-10 #index with maximum Isum
iwhere=-10 #index with maximum Isum
for i, z in enumerate(zarr):
for i, z in enumerate(zarr):
    u_vec = np.real(V[:, indx]*np.exp(1 j*(ck*z))+np.conjugate(V[:, indx]) *np.exp
    u_vec = np.real(V[:, indx]*np.exp(1 j*(ck*z))+np.conjugate(V[:, indx]) *np.exp
        (-1j *(ck*z)))
        (-1j *(ck*z)))
    egv.vector().set_local(u_vec)
    egv.vector().set_local(u_vec)
    euvw, ep = split(egv)
    euvw, ep = split(egv)
    eu,ev,ew = split(euvw)
    eu,ev,ew = split(euvw)
    u_vec_dz = np.real ((1 j*ck) *(V[:, indx]*np.exp(1 j*(ck*z))-np.conjugate(V[:,
    u_vec_dz = np.real ((1 j*ck) *(V[:, indx]*np.exp(1 j*(ck*z))-np.conjugate(V[:,
        indx])*np.exp(-1j*(ck*z))))
        indx])*np.exp(-1j*(ck*z))))
    egv_dz.vector().set_local(u_vec_dz)
    egv_dz.vector().set_local(u_vec_dz)
    euvw_dz,ep_dz = split(egv_dz)
    euvw_dz,ep_dz = split(egv_dz)
    eu_dz,ev_dz,ew_dz= split(euvw_dz)
    eu_dz,ev_dz,ew_dz= split(euvw_dz)
    euvw_par = dot(euvw, self.uvw0)*self.uvw0 /( dot(self.uvw0, self.uvw0))
    euvw_par = dot(euvw, self.uvw0)*self.uvw0 /( dot(self.uvw0, self.uvw0))
    eu_par,ev_par,ew_par = euvw_par
    eu_par,ev_par,ew_par = euvw_par
    euvw_orth = euvw - euvw_par
    euvw_orth = euvw - euvw_par
    eu_orth,ev_orth,ew_orth = euvw_orth
```

    eu_orth,ev_orth,ew_orth = euvw_orth
    ```


```

        dx
    ```
        dx
    D = assemble(D)
```

    D = assemble(D)
    ```
```

I1 = - eu_orth * (eu_orth * self.u0.dx(0) + ev_orth * self.u0.dx(1)) \
- ev_orth * (eu_orth * self.v0.dx(0) + ev_orth * self.v0.dx(1))
- ew_orth * (eu_orth * self.w0.dx(0) + ev_orth * self.w0.dx(1))
I1 = assemble(I1*dx)
I2 = - eu_par * (eu_orth * self.u0.dx(0) + ev_orth * self.u0.dx(1)) \
- ev_par * (eu_orth * self.v0.dx(0) + ev_orth * self.v0.dx(1))
- ew_par * (eu_orth * self.w0.dx(0) + ev_orth * self.w0.dx(1))
I2 = assemble(I2*dx)
I3 = - eu_orth * (eu_par * self.u0.dx(0) + ev_par * self.u0.dx(1)) \
- ev_orth * (eu_par * self.v0.dx(0) + ev_par * self.v0.dx(1))
- ew_orth * (eu_par * self.w0.dx(0) + ev_par * self.w0.dx(1))
I3 = assemble(I3*dx)
I4 = - eu_par * (eu_par * self.u0.dx(0) + ev_par * self.u0.dx(1)) \
- ev_par * (eu_par * self.v0.dx(0) + ev_par * self.v0.dx(1)) \
- ew_par * (eu_par * self.w0.dx(0) + ev_par * self.w0.dx(1))
I4 = assemble(I4*dx)
Isum = I 1 +I2+I 3+I4
if(Isum>Imax):
Imax = Isum
iwhere = i
D_int += D*delta_z
I1_int += I1*delta_z
I2_int += I2*delta_z
I3_int += I3*delta_z
I4_int += I 4*delta_z
egvfolder = self.calcdir+"/EGV_Re_{:08.4f}_k_{:08.4f}".format(Re,ck)
if not os.path.exists(egvfolder):
os.mkdir(egvfolder)
f2=open(egvfolder+" /ENERGIES" , 'w')
f2.write('\# D I1 I2 I3 I4 \n')
f2.write('{:.6e} {:.6e} {:.6e} {:.6e} {:.6e} '.format(D_int,I1_int,I2_int,
I3_int,I4_int))
f2.close()
if(lplot):
\#PLOT THE FLOW WITH THE MAXIMAL ENERGY GAIN AND THE ENERGY CONTRIBUTIONS
z=zarr[iwhere]
u_vec = np.real(V[:,indx]*np.exp (1 j * (ck*z))+np.conjugate(V[:, indx]) *np.exp
(-1j * (ck*z)))
egv.vector().set_local(u_vec)
euvw,ep = split(egv)
eu,ev,ew = split(euvw)
euvw_par = dot(euvw,self.uvw0)*self.uvw0 /(dot(self.uvw0,self.uvw0))
eu_par,ev_par,ew_par = euvw_par
euvw_orth = euvw - euvw_par
eu_orth,ev_orth,ew_orth = euvw_orth
u_vec_dz = np.real ((1 j*ck)*(V[:, indx]*np.exp(1 j * (ck*z))-np.conjugate(V[:,
indx])*np.exp(-1j*(ck*z))))
egv_dz.vector().set_local(u_vec_dz)
euvw_dz,ep_dz= split(egv_dz)
eu_dz,ev_dz,ew_dz= split(euvw_dz)
euvw_par = dot(euvw,self.uvw0)*self.uvw0 / (dot(self.uvw0, self.uvw0))
eu_par,ev_par,ew_par = euvw_par
euvw_orth = euvw - euvw_par
eu_orth,ev_orth,ew_orth = euvw_orth
D = (ew.dx(1)-ev_dz)**2 + (eu_dz-ew.dx(0))**2. + (ev.dx(0)-eu.dx (1))**2
I1 = - eu_orth * (eu_orth * self.u0.dx(0) + ev_orth * self.u0.dx(1)) \
_ ev_orth * (eu_orth * self.v0.dx(0) + ev_orth * self.v0.dx(1)) \
- ew_orth * (eu_orth * self.w0.dx(0) + ev_orth * self.w0.dx(1))

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```

    I2 = - eu_par * (eu_orth * self.u0.dx(0) + ev_orth * self.u0.dx(1)) \
        - ev_par * (eu_orth * self.v0.dx(0) + ev_orth * self.v0.dx(1)) \
        - ew_par * (eu_orth * self.w0.dx(0) + ev_orth * self.w0.dx(1))
        I3 = - eu_orth * (eu_par * self.u0.dx(0) + ev_par * self.u0.dx(1)) \
        - ev_orth * (eu_par * self.v0.dx(0) + ev_par * self.v0.dx(1)) \
        - ew_orth * (eu_par * self.w0.dx(0) + ev_par * self.w0.dx(1))
        I4 = - eu_par * (eu_par * self.u0.dx(0) + ev_par * self.u0.dx(1)) \
        - ev_par * (eu_par * self.v0.dx(0) + ev_par * self.v0.dx(1)) \
        - ew_par * (eu_par * self.w0.dx(0) + ev_par * self.w0.dx(1))
        Isum = I 1 +I2+I3+I4
        IDsum = Isum + D
        #####Create files for storing solution
        V2 = FunctionSpace(self.mesh,self.P1)
        for i, en in zip(['D','I1','I2','I3','I4','Isum ','IDsum'],[D, I1,I2,I3,I4,
        Isum,IDsum]):
        filename=egvfolder+"/"+i+" .pvd"
        Ifile=File(filename)
        temp = project(en,V2)
        temp.rename(i, "")
        Ifile << temp
        ###RENAME THE FIELD TO BE BE NAMED vel AND p
        ufilename = egvfolder+"/u.pvd"
        ufile = File(ufilename)
        egv.rename("vel","")
        ufile << egv.sub(0)
        pfilename=egvfolder+"/p.pvd"
        pfile = File(pfilename)
        egv.rename("pressure","")
        pfile << egv.sub(1)
    #########SAVING DONE
    return sigma,omega
    def linearstab_MORE_EV(self,Re, karr,nr_EV,lplot=False, enanalysis=False):
    #THE PERTURBATION-FUNCTIONS
    uvwp_p = TrialFunction(self.W)
    uvec_p,p_p = split(uvwp_p)
    u_p,v_p,w_p = split(uvec_p)
    #THE BOUNDARY CONDITIONS FOR THE PERTURBATION
    ubcN_p = DirichletBC(self.W.sub(0), Constant((0.,0.,0.)), self.bcN)
    ubcSEW_p= DirichletBC(self.W.sub(0),Constant((0.,0.,0.)), self.bcSEW)
    bcs_p=[ubcSEW_p,ubcN_p]
    k=Constant(0.1)
    sigma_low=np.zeros(np.size(karr))
    omega_low=np.zeros(np.size(karr))
    sigma=np.zeros([np.size(karr),nr_EV])
    omega=np.zeros([np.size(karr),nr_EV])
    for i,ck in enumerate(karr):
        k.assign(ck)
        Fp_real= \
            self.du*self.u0*u_p.dx(0)*dx+self.du*self.v0*u_p.dx(1)*dx+self.du*u_p*
                self.u0.dx(0)*dx+self.du*v_p*self.u0.dx(1)*dx+\
            self.du*p_p.dx(0)*dx+self.du.dx(0)*u_p.dx(0)*dx+self.du.dx(1)*u_p.dx (1)*
                dx+self.du*k**2.*u_p*dx+\
            self.dv*self.u0*v_p.dx(0)*dx+self.dv*self.v0*v_p.dx(1)*dx+self.dv*u_p*
                self.v0.dx (0)*dx+self.dv*v_p*self.v0.dx (1)*dx+\
            self.dv*p_p.dx(1)*dx+self.dv.dx(0)*v_p.dx(0)*dx+self.dv.dx(1)*v_p.dx (1)*
                dx+self.dv*k**2.*v_p*dx+\
    ```
```

    self.dw*self.u0*w_p.dx(0)*dx+self.dw*self.v0*w_p.dx(1)*dx+self.dw*u_p*
    self.w0.dx(0)*dx+self.dw*v_p*self.w0.dx(1)*dx+\
    self.dw.dx(0)*w_p.dx(0)*dx+self.dw.dx(1)*w_p.dx (1)*dx+self.dw*k**2.*w_p*
        dx+\
    self.dp*u_p.dx(0)*dx+self.dp*v_p.dx(1)*dx
    
# 

# 

# 

Fp_imag=\
self.du*self.w0*k*u_p*dx+self.dv*self.w0*k*v_p*dx+self.dw*self.w0*k*
w_p*dx+self.dw*k*p_p*dx+self.dp*k*w_p*dx
B_MAT = \
self.du*u_p*dx+self.dv*v_p*dx+self.dw*w_p*dx

# 

Ar = PETScMatrix ()
assemble(Fp_real, tensor=Ar)
[bc.apply(Ar) for bc in bcs_p]
Ai = PETScMatrix()
assemble(Fp_imag, tensor=Ai)
[bc.apply(Ai) for bc in bcs_p]
M = PETScMatrix()
assemble(B_MAT, tensor=M)
\#\bc.apply(M) for bc in bcs_p]

# 

bcinds= []
for bc in bcs_p:
bcdict = bc.get_boundary_values()
bcinds.extend(bcdict.keys())

# This just converts PETSc to CSR

Ar=sp.csr_matrix(Ar.mat().getValuesCSR()[::-1])
Ai = sp.csr_matrix(Ai.mat().getValuesCSR()[::-1])
M=sp.csr_matrix (M.mat().getValuesCSR()[::-1])

# Create shift matrix

\#shift = 1.2345e10*np.ones(len(bcinds))
\#S = sp.csr_matrix((shift, (bcinds, bcinds)), shape=Ar.shape)
if (nr_EV<10):
v, V = eigs (Ar+1.j*Ai, 10, M, sigma=-10)
else:
v, V}=\operatorname{eigs}(\textrm{Ar}+1.j*Ai, 10, M, sigma=-10
sigma_low[i],omega_low[i]=np.sort(v)[0].real, np.sort(v)[0].imag
print('Re={}, k={} lowest_sigma = {}, omega = {}'.format(Re,ck, sigma_low
[i],omega_low[i]))
print('OTHER EIGENVALS : \n')
\#ARRAY FOR A MAPPING OF SIGMA
maparr=np.argsort(v)
for ij in range(nr_EV):
sigma[i, ij],omega[i, ij]=np.sort(v)[ij].real, np.sort(v)[ij].imag
print('sigma = {} , omega = {} \n'.format(sigma[i,ij],omega[i,ij]))
if(enanalysis):
\#\#SAVE THE RESULTING FLOW FUNCTIONS
egv = Function(self.W)
egv_dz= Function(self.W)
\#\#index of lowest sigma
for isigma in range(nr_EV):
indx = maparr[isigma]
\#STORE REAL AND IMAGINARY PART OF THE EIGENVECTOR
intsteps=100

```
```

zarr = np.linspace(0., 2.*np.pi/ck,intsteps)
delta_z = zarr[1]-zarr[0]
D int=0.
I1_int=0.
I2_int=0.
I3_int=0.
I4_int=0.
Isum_int=0.
Imax = -1.e99
iwhere=-10 \#index with maximum Isum
for i, z in enumerate(zarr):
u_vec = np.real(V[:,indx]*np.exp(1j * (ck*z))+np.conjugate(V[:, indx]) *np.
exp(-1j*(ck*z)))
egv.vector().set_local(u_vec)
euvw,ep = split(egv)
eu,ev,ew = split(euvw)
u_vec_dz = np.real((1 j*ck)*(V[:,indx]*np.exp(1j j (ck*z))-np.conjugate(V[:,
indx])*np.exp(-1j *(ck*z))))
egv_dz.vector().set_local(u_vec_dz)
euvw_dz,ep_dz= split(egv_dz)
eu_dz,ev_dz,ew_dz = split(euvw_dz)
euvw_par = dot(euvw, self.uvw0)*self.uvw0 /(dot(self.uvw0, self.uvw0))
eu_par,ev_par,ew_par = euvw_par
euvw_orth = euvw - euvw_par
eu_orth,ev_orth,ew_orth = euvw_orth
D = ((ew.dx (1)-ev_dz)**2 + (eu_dz-ew.dx (0))**2. + (ev.dx (0)-eu.dx (1))**2)
*dx
D = assemble(D)
I1 = - eu_orth * (eu_orth * self.u0.dx(0) + ev_orth * self.u0.dx(1)) \
- ev_orth * (eu_orth * self.v0.dx(0) + ev_orth * self.v0.dx(1))
_ ew_orth * (eu_orth * self.w0.dx(0) + ev_orth * self.w0.dx(1))
I1 = assemble(I1 *dx)
I2 = - eu_par * (eu_orth * self.u0.dx(0) + ev_orth * self.u0.dx(1)) \
- ev_par * (eu_orth * self.v0.dx(0) + ev_orth * self.v0.dx(1))
- ew_par * (eu_orth * self.w0.dx(0) + ev_orth * self.w0.dx(1))
I2 = assemble(I2*dx)
I3 = - eu_orth * (eu_par * self.u0.dx(0) + ev_par * self.u0.dx(1)) \
- ev_orth * (eu_par * self.v0.dx(0) + ev_par * self.v0.dx(1)) \
- ew_orth * (eu_par * self.w0.dx(0) + ev_par * self.w0.dx(1))
I3 = assemble(I3*dx)
I4 = - eu_par * (eu_par * self.u0.dx(0) + ev_par * self.u0.dx(1)) \
- ev_par * (eu_par * self.v0.dx(0) + ev_par * self.v0.dx(1)) \
- ew_par * (eu_par * self.w0.dx(0) + ev_par * self.w0.dx(1))
I4 = assemble(I4*dx)
Isum = I 1 +I2+I 3+I4
if(Isum>Imax) :
Imax = Isum
iwhere = i
D_int += D*delta_z
I1_int += I1*delta_z
I2_int += I2*delta_z
I3_int += I3*delta_z
I4_int += I 4*delta_z
egvfolder = self.calcdir+"/EGV_Re_{:08.4f}_k_{:08.4f}_EV_{:03d}".format(Re
,ck,isigma)
if not os.path.exists(egvfolder):
os.mkdir(egvfolder)
f2=open(egvfolder+" /ENERGIES".format(isigma), 'w')

```
```

f2.write('\# D I1 I2 I3 I4 \n')
f2.write('{:.6e} {:.6e} {:.6e} {:.6e} {:.6e} '.format(D_int,I1_int,I2_int,
I3_int,I4_int))
f2.close()
if(lplot):
\#PLOT THE FLOW WITH THE MAXIMAL ENERGY GAIN AND THE ENERGY CONTRIBUTIONS
z=zarr[iwhere]
u_vec = np.real(V[:, indx]*np.exp(1 j*(ck*z))+np.conjugate(V[:, indx])*np.
exp(-1j *(ck*z)))
egv.vector().set_local(u_vec)
euvw,ep = split(egv)
eu,ev,ew = split(euvw)
euvw_par = dot(euvw, self.uvw0)*self.uvw0 /( dot(self.uvw0, self.uvw0))
eu_par,ev_par,ew_par = euvw_par
euvw_orth = euvw - euvw_par
eu_orth,ev_orth,ew_orth = euvw_orth
u_vec_dz = np.real ((1 j*ck)*(V[:,indx]*np.exp(1 j*(ck*z))-np.conjugate(V[:,
indx])*np.exp(-1j*(ck*z))))
egv_dz.vector().set_local(u_vec_dz)
euvw_dz,ep_dz= split(egv_dz)
eu_dz,ev_dz,ew_dz = split(euvw_dz)
euvw_par = dot(euvw,self.uvw0)*self.uvw0 /( dot(self.uvw0, self.uvw0))
eu_par,ev_par,ew_par = euvw_par
euvw_orth = euvw - euvw_par
eu_orth,ev_orth,ew_orth = euvw_orth
D = (ew.dx(1)-ev_dz)**2 + (eu_dz-ew.dx(0))**2. + (ev.dx(0)-eu.dx(1))**2
I1 = - eu_orth * (eu_orth * self.u0.dx(0) + ev_orth * self.u0.dx(1)) \
_ ev_orth * (eu_orth * self.v0.dx(0) + ev_orth * self.v0.dx(1)) \
- ew_orth * (eu_orth * self.w0.dx(0) + ev_orth * self.w0.dx(1))
I2 = - eu_par * (eu_orth * self.u0.dx(0) + ev_orth * self.u0.dx(1)) \
- ev_par * (eu_orth * self.v0.dx(0) + ev_orth * self.v0.dx(1)) \
- ew_par * (eu_orth * self.w0.dx(0) + ev_orth * self.w0.dx(1))
I3 = - eu_orth * (eu_par * self.u0.dx(0) + ev_par * self.u0.dx(1)) \
- ev_orth * (eu_par * self.v0.dx(0) + ev_par * self.v0.dx(1)) \
- ew_orth * (eu_par * self.w0.dx(0) + ev_par * self.w0.dx(1))
I4 = - eu_par * (eu_par * self.u0.dx(0) + ev_par * self.u0.dx(1)) \
- ev_par * (eu_par * self.v0.dx(0) + ev_par * self.v0.dx(1)) \
- ew_par * (eu_par * self.w0.dx(0) + ev_par * self.w0.dx(1))
Isum = I1 +I 2+I 3+I4
IDsum = Isum + D
\#\#\#\#\#Create files for storing solution
V2 = FunctionSpace(self.mesh, self.P1)
for i, en in zip(['D','I1','I2','I3','I4','Isum','IDsum'],[D, I1, I2,I3,I4,
Isum,IDsum]):
filename=egvfolder+" / "+i+".pvd"
Ifile=File(filename)
temp = project(en,V2)
temp.rename(i, " " )
Ifile << temp
\#\#\#RENAME THE FIELD TO BE BE NAMED vel AND p
ufilename = egvfolder+"/u.pvd"
ufile = File(ufilename)
egv.rename(" vel", " " )
ufile << egv.sub(0)
pfilename=egvfolder+"/p.pvd"
pfile = File(pfilename)
egv.rename(" pressure", "")
pfile << egv.sub(1)

```
```

\#\#\#\#\#\#\#\#\#\#\#SAVING DONE
return sigma_low,omega_low,sigma,omega
def mymeshrefine(self):
\#parameters["num_threads"] = 1
parameters["mesh_partitioner"]= 'ParMETIS'
\#REFINE CLOSE TO THE BORDER
\#TRY 3 REFINEMENTS IN THE BEGINNING
\#@30% 15% 5% of the box
dist_pc=np.array ([0.3,0.15,0.05])
distx_left = -1./2.+ dist_pc*1.
distx_right = 1./2.- dist_pc*1.
disty_bottom = -self.Gamma/2.+ dist_pc*self.Gamma
disty_top = self.Gamma/2.-dist_pc*self.Gamma
for i in range(len(dist_pc)):
cell_markers = CellFunction("bool", self.mesh)
cell_markers.set_all(False)
for cell in cells(self.mesh):
p = cell.midpoint()
if ((p.x()<distx_left[i]) or
(p.x()>distx_right[i]) or
(p.y()<disty_bottom[i]) or
(p.y()>disty_top[i])):
cell_markers[cell]=True
self.mesh=refine(self.mesh,cell_markers)
def getsignchange(self, inarr):
nr=0
change=[]
indices=[]
for i in range(np.size(inarr)-1):
if (inarr[i]>=0 and inarr [i+1]<0):
nr}+=
change.append(1)
indices.append(i)
elif(inarr[i]<=0 and inarr[i+1]>0):
nr+=1
change.append (-1)
indices.append(i)
return nr, np.array(change), np.array(indices)
def find_nearest(self, array, value):
array = np.asarray (array)
idx = (np.abs(array - value)).argmin()
return idx, array[idx]
def plot_k_sigma(self,Re, filename):
plotfile=open(filename,'r')
data=plotfile.readlines()
data_arr=np.zeros([len(data),2])
for i, line in enumerate(data):
data_arr[i,0], data_arr[i,1]= float(line.split()[0]), float(line.split ()[1])
\#sort the array
temp = np.argsort(data_arr,0) [:,0]
sorted_arr=data_arr[temp]
\#SET MATPLOTLIB TeX
plt.rc('font',**{'family':'serif','serif':['Times']})
plt.rc('text',usetex=True)
def cm2inch(value):

```
```

    return value/2.54
    fig,ax = plt.subplots(1, figsize=(cm2inch(13.8), cm2inch(7.0)))
    ax.plot(sorted_arr[:,0], sorted_arr[:, 1], c='r', linestyle='-')
    ax.grid(True, which='both', ls="--" , lw = 0.15)
    ax.set_title('Stability for Re = {}'.format(Re))
    ax.title.set_weight('bold')
    ax.set_xlim([0, 10.])
    ax.set_xlabel(r"k",labelpad=1.)
    ax.set_ylabel(r"$\sigma$", labelpad=1.)
    savename=self.calcdir+'/'+'Re_{:07.1f}.pdf'.format(Re)
    plt.savefig(savename,format='pdf',dpi=fig.dpi)
    def readdataset(self,Gamma, angle,Re):
folder='Gamma_{:07.3f}_alpha_{:05.1f}'..format (Gamma, angle)
filename=folder+'/'+'Re'+'_{:08.3 f }'. format(Re)
Refile=open(filename,'r')
lines=Refile.readlines()
karr=np.zeros(len(lines))
sigma_arr=np.zeros(len(lines))
omega_arr=np.zeros(len(lines))
for i, line in enumerate(lines):
karr[i] = float(line.split()[0])
sigma_arr[i] = float(line.split()[1])
omega_arr[i] = float(line.split()[2])
return karr,sigma_arr,omega_arr
def get_kneutral(self,Gamma, alpha, Re):
karr,sigma_arr,omega_arr=self.readdataset (Gamma, alpha, Re)
nr, changearr, indices=self.getsignchange(sigma_arr)
if(nr=0):
return 0
else:
return karr[indices],sigma_arr[indices],omega_arr[indices]
\#A FUNCTION WHERE WE COMPARE DIFFERENT CURVES
\#plotarr has to be a dictionairy that provides the Gamma,Re, angle values
def compareplot(self, plotarr, show=True):
\#SET MATPLOTLIB TeX
plt.rc('font',**{'family''''serif','serif':['Times']})
plt.rc('text',usetex=True)
def cm2inch(value):
return value/2.54
fig,ax = plt.subplots(1, figsize=(cm2inch(13.8) , cm2inch (7.0)) )
ax.grid(True, which='both', ls='--" , lw = 0.15)
colors = ['\#0000ff','\#ff0000','\#009933','\#cc0099','\#ff9900', '\#0099cc',\
'\#009999']
for i in range(len(plotarr)):
Gamma=plotarr[i][ 'Gamma']
Re= plotarr[i]['Re']
angle = plotarr[i]['angle']
label = r'$\alpha={:5.2f} \Gamma={:5.2f} Re={:8.2f}$'.format(angle,Gamma,Re)
karr,sigma_arr,omega_arr=self.readdataset (Gamma, angle, Re)
\#SORT THE ARRAYS
sigma_arr=sigma_arr[np.argsort (karr)]
omega_arr=omega_arr[np.argsort(karr)]
karr = np.sort(karr)
ax.plot(karr,sigma_arr,c=colors[i], linestyle='-', label=label)
ax.set_xlabel(r"k", labelpad=1.)
ax.set_ylabel(r"$\sigma$", labelpad=1.)

```
```

    ax.legend()
    if(show):
        plt.show()
    else:
    plt.savefig('TEMPPLOT.pdf',format='pdf',dpi=fig.dpi)
    def analyze_k_n(self,Re,relax_param,k1,k2,ngrid):
print('RUNNING ANALYZE_K WITH REYNOLDS: {} \n k1 = {} k2 = {}'.format(Re,k1,
k2))
filename=self.calcdir+'/'+'Re_k'+'_{:08.3f}'.format(Re)
Refile=open(filename,'w')
karr=np.linspace(k1,k2,3)
nx=ngrid
ny=ngrid
self.getbaseflow(Re,nx,ny)
sigma,omega=self.linearstab(Re, karr)
for line in range(len(sigma)):
Refile.write('{:10g} {:10g} {:10g} \n'.format(karr[line],sigma[line],
omega[line]))
nr,changearr, indices=self.getsignchange(sigma)
Refile.close()
def gamma_angle_Re(gammaarr, anglearr, Rearr,relax_param_arr):
for Gamma in gammaarr:
for angle in anglearr:
print(',,
%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%
CALCULATING GAMMA = {:07.3f} AND ANGLE = {:05.1 f }
%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%, ' , '. format(Gamma, angle ) )
folder='Gamma_{:07.3 f }_alpha_ {:05.1f}'.format(Gamma, angle)
cav=mycav(Gamma, angle, calcdir=folder)
for Re,relax_param in zip(Rearr,relax_param_arr):
cav.analyze(Re,relax_param)
def RcAnalysis(gammaarr, anglearr, Reminarr, Remaxarr):
for Gamma in gammaarr:
for angle in anglearr:
print(',,
%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%
ReC analysis: GAMMA = {:07.3f} AND ANGLE = {:05.1f }
%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%% ' ' , format(Gamma, angle ) )
folder='Gamma_{:07.3 f }_alpha_{:05.1f}'.format(Gamma, angle)
cav=mycav(Gamma, angle, calcdir=folder)
Re_low=Reminarr [0]
Re_high=Remaxarr [0]
cav.findRe_c(Re_low,Re_high)
def RcAnalysis_MORE_EV(gammaarr,anglearr,Reminarr,Remaxarr,nr_EV_arr,kmin,kmax,
nr_k):
for Gamma in gammaarr:
for angle in anglearr:
print(',,
%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%
ReC analysis: GAMMA ={:07.3 f} AND ANGLE ={:05.1f}
%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%, , ', format (Gamma, angle )
folder='Gamma_{:07.3 f }_alpha_{:05.1f}'. format(Gamma, angle)
cav=mycav(Gamma, angle, calcdir=folder)
Re_low=Reminarr [0]
Re_high=Remaxarr [0]
nr_EV=nr_EV_arr [0]

```
```

    cav.findRe_c_MORE_EV(Re_low,Re_high,nr_EV,kmin, kmax, nr_k)
    if __name___',_main__'
print('HELLO')

```

\section*{D.1.2 Plotting script}
```

from fenics import *
import matplotlib.pyplot as plt
import scipy.sparse as sp
from scipy.sparse.linalg import eigs
import numpy as np
import os
import sys
class mycav:
def__init__(self,Gamma, alpha, calcdir=None):
self.Gamma-Gamma
self.alpha=alpha
if (calcdir!=None):
self.calcdir=calcdir
if not os.path.exists(calcdir):
os.mkdir(calcdir)
def analyze(self,Re,relax_param):
print('RUNNING ANALYZE WITH REYNOLDS: {}'.format(Re))
print('1st RUN ——> coarse GRID')
filename=self.calcdir+'/'+'Re'+'_{:08.3 f }'. format(Re)
Refile=open(filename, 'w')
karr=np.linspace (0.001,30,30)
nx=70
ny=70
self.getbaseflow(Re, nx, ny, relax_param)
sigma,omega=self.linearstab(Re, karr)
for line in range(len(sigma)):
Refile.write('{:10g} {:10g} {:10g} \n'.format(karr[line],
sigma[line],omega[line]))
nr, changearr, indices=self.getsignchange(sigma)
print('FOUND {} SIGN CHANGES'.format (nr))
\#1 st REFINEMENT OF THE MESH FOR THE CRITICAL k-VALUES
if ( nr>0) :
nx=75
ny=75
self.getbaseflow(Re, nx, ny, relax_param)
for i in indices:
k1=karr[i ] ; k2=karr [i +1]
conv=100
kdiff=10
run=0
while(conv>1e-3 and kdiff > 0.1):
run+=1
print('LOOKING IN THE VICINITY OF k= {}'.format(k1))
k_refine=np.linspace(k1,k2,5)
sigma2,omega2=self.linearstab(Re, k_refine)
nr2, changearr2, indices2=self.getsignchange(sigma2)
if (nr2==0 and run>1):
k1=karr [i - 1]
k2=karr [i+2]
elif(nr2==0 and run==1):

```
```

            break
        else:
            k1=k_refine[indices2 [0]]
            k2=k_refine[indices2[0]+1]
        kdiff=abs(k2-k1)
        conv=abs(self.find_nearest(sigma2,0)[1])
        for line in range(len(sigma2)):
            Refile.write('{:10g} {:10g} {:10g} \n'.format(
                k_refine[line], sigma2[line],omega2[line]))
        print('SIGMA(k_crit) before 2nd REFINEMENT: {}'.format(sigma2[
        indices2[0]]))
        #EXTRACT THE VALUE CLOSEST TO o
        kchoose=k_refine[self.find_nearest(sigma2,0) [0]]
        #2nd REFINEMENT TO CHECK FOR CONVERGENCE
        nx=85
        ny=85
        self.getbaseflow(Re, nx, ny, relax_param)
        sigma2,omega2=self.linearstab (Re, np.asarray ([kchoose]))
        print('SIGMA(k_crit) after 2nd REFINEMENT: {}'.format(sigma2
        [0]))
        Refile.write('{:10g} {:10g} {:10g} \n'.format(kchoose,
        sigma2[0],omega2[0]))
    Refile.close()
    self.plot_k_sigma(Re,filename)
    def findRe_c(self,Re_low, Re_high):
resultname=self.calcdir+'/'+'REc_Gamma_{:5.2f}_alpha_{:5.2 f }'.format(
self.Gamma, self.alpha)
Resultfile=open(resultname, 'w')
karr=np.linspace (0.001,30,30)
nx=75
ny=75
Rearr=np.array ([Re_low, Re_high])
Remid=(Re_low+Re_high)/2.
while (np.min(abs(Rearr-Remid))>1.):
print('RUNNING findRe_c WITH REYNOLDS: {}'.format(Remid))
filename=self.calcdir+'/'+'Re_crit'+'_{:08.3 f }'.format(Remid)
Refile=open(filename, 'w')
if (Remid<500):
relax_param=0.5
elif(Remid>=500 and Remid < 1200):
relax_param=0.3
else:
relax_param=0.1
self.getbaseflow(Remid,nx, ny, relax_param)
sigma,omega=self.linearstab(Remid, karr)
for line in range(len(sigma)):
Refile.write('{:10g} {:10g} {:10g} \n'.format(karr[line],
sigma[line],omega[line]))
nr, changearr, indices=self.getsignchange(sigma)
Resultfile.write('{:7.2f} {:2d} \n'.format(Remid,nr))
print('FOUND {} SIGN CHANGES'.format(nr))
if (nr>0):
Rearr[1]= Remid
elif(nr==0):
Rearr [0]= Remid
Remid=(Rearr[0]+Rearr[1])/2.
Refile.close()

```
```

    Resultfile.close()
    def getbaseflow(self,Re, nx, ny, relax_param):
\#CREATE THE MESH
self.mesh=RectangleMesh(Point(-self.Gamma/2., - 0.5), Point(self.Gamma
/2.,0.5),nx,ny)
\#REFINE THE MESH HERE
self.mymeshrefine()
\#DEFINE TRIAL AND TEST FUNCTIONS
self.P2 = VectorElement('P',triangle, degree=2,dim=3)
self.P1 = FiniteElement('P',triangle, degree=1)
self.element = MixedElement([self.P2,self.P1])
self.W= FunctionSpace(self.mesh, self.element)
self.duvw,self.dp = TestFunctions(self.W)
self.du,self.dv,self.dw = split(self.duvw)
\#THE FUNCTIONS FOR THE FORMULATION
uvwp = Function(self.W)
uvw,p = split(uvwp)
u,v,w = split(uvw)
\#THE FUNCTIONS FOR THE STEADY STATE SOLUTION
self.uvwp0 = Function(self.W)
self.uvw0,p0 = split(self.uvwp0)
self.u0,self.v0,self.w0 = split(self.uvw0)
Gamma=self.Gamma
tol=1e-14
\#DEFINE THE BOUNDARIES
class BoundN(SubDomain):
def inside(self,x,on_boundary):
return on boundary and near (x[1],0.5, tol)
class BoundSEW(SubDomain):
def inside(self,x,on_boundary):
return on_boundary and (near(x[1], -0.5, tol) or
near(x[0], -Gamma/2., tol)
or near(x[0],Gamma/2., tol))
self.bcN=BoundN()
self.bcSEW=BoundSEW()
ubcN = DirichletBC(self.W.sub(0), Constant((Re*np.cos(self.alpha/180.*np
.pi) ,0., Re*np.sin(self.alpha/180.*np.pi))), self.bcN)
ubcSEW= DirichletBC(self.W.sub(0), Constant((0., 0., 0.)), self.bcSEW)
bcs=[ubcSEW,ubcN]
\#\#\#NS-equation
F}=\mathrm{ self.du*u*u.dx (0)*dx+self.du*v*u.dx (1)*dx+inner(grad (self.du),grad(
u))*dx+self.du*p.dx(0)*dx +\
self.dv*u*v.dx (0)*dx+self.dv*v*v.dx (1)*dx+inner(grad(self.dv),grad(
v))*dx+self.dv*p.dx (1)*dx +\
self.dw*u*w.dx (0)*dx+self.dw*v*w.dx(1)*dx+inner(grad(self.dw),grad(
w))*dx +\
self.dp*u.dx(0)*dx+self.dp*v.dx (1)*dx
J=derivative(F,uvwp)
M=u.dx (0)*dx+v.dx (1)*dx
problem = NonlinearVariationalProblem(F, uvwp, bcs, J=J)
solver = AdaptiveNonlinearVariationalSolver(problem,M)
\#solver = NonlinearVariationalSolver(problem)
prm = solver.parameters

```
    prm["nonlinear_variational_solver"]["newton_solver"]["
        absolute_tolerance" \(]=1 \mathrm{E}-8\)
    prm["nonlinear_variational_solver"]["newton_solver"]["
        relative_tolerance" \(]=1 \mathrm{E}-8\)
    prm["nonlinear_variational_solver"]["newton_solver"]["
        maximum_iterations"] = 350
    prm["nonlinear_variational_solver"]["newton_solver"]["
        relaxation_parameter"]=relax_param
    solver_tolerance \(=1 \mathrm{E}-8\)
    solver.solve (solver_tolerance)
    self.uvwp0.assign (uvwp)
def linearstab (self, Re, karr) :
    \#THE PERTURBATION-FUNCTIONS
    uvwp_p \(=\) TrialFunction (self.W)
    uvec_p,p_p = split (uvwp_p)
    u_p, v_p,w_p = split (uvec_p)
    \#THE BOUNDARY CONDITIONS FOR THE PERTURBATION
    \(u b c N \_p=\) DirichletBC(self.W.sub(0), Constant ( \(\left.0 ., 0 ., 0.\right)\) ), self.bcN)
    ubcSEW_p= DirichletBC (self.W.sub(0), Constant ( \(0 ., 0 ., 0\).\() ), self.bcSEW)\)
    bcs_p=[ubcSEW_p,ubcN_p]
    \(\mathrm{k}=\) Constant (0.1)
    \(\operatorname{sigma}=n \mathrm{p} \cdot \operatorname{zeros}(\mathrm{np} . \operatorname{size}(\) karr \())\)
    omega=np.zeros (np.size(karr))
    for \(\mathrm{i}, \mathrm{ck}\) in enumerate(karr):
        k. assign (ck)
        Fp_real= \}
            self.du*self.u0*u_p.dx \((0) * d x+\) self.du*self.v0*u_p.dx(1)*dx+self.
            \(d u * u \_p * s e l f . u 0 . d x(0) * d x+s e l f . d u * v \_p * s e l f . u 0 . d x(1) * d x+\backslash\)
        self.du*p_p.dx(0)*dx+self.du.dx(0)*u_p.dx(0)*dx+self.du.dx(1)*
            \(u \_p . d x(1) * d x+\) self.du \(*\) k \(* * 2 \cdot * u \_p * d x+\backslash\)
        self.dv*self.u \(0 *\) v_p. \(d x(0) * d x+\) self. \(d v *\) self.v \(0 * v \_p . d x(1) * d x+\) self.
            \(d v * u \_p * s e l f . v 0 . d x(0) * d x+s e l f . d v * v \_p * s e l f . v 0 . d x(1) * d x+\backslash\)
        self. \(d v * p \_p . d x(1) * d x+s e l f . d v . d x(0) * v \_p . d x(0) * d x+s e l f . d v . d x(1) *\)
            v_p. \(\mathrm{dx}(1) * \mathrm{dx}+\mathrm{self} \cdot \mathrm{dv} * \mathrm{k} * * 2 . * \mathrm{v} \_\mathrm{p} * \mathrm{dx}+\backslash\)
        self.dw \(\operatorname{self.u0*w\_ p.dx(0)*dx+self.dw*self.v0*w\_ p.dx(1)*dx+self.~}\)
            \(d w * u \_p * s e l f . w 0 . d x(0) * d x+s e l f . d w * v \_p * s e l f . w 0 . d x(1) * d x+\backslash\)
        self.dw. dx (0) *w_p. dx (0) \(* \mathrm{dx}+\mathrm{self} . \mathrm{dw} . \mathrm{dx}(1) * \mathrm{w} \_\mathrm{p} . \mathrm{dx}(1) * \mathrm{dx}+\mathrm{self} . \mathrm{dw} * \mathrm{k}\)
                **2.*w_p*dx+\}
            self.dp*u_p.dx \((0) * d x+\) self. \(d p * v \_p . d x(1) * d x\)
        \#
        \#
        \#
        Fp_imag= \}
                        self.du*self.w0 \(* \mathrm{k} * \mathrm{u} \_\mathrm{p} * \mathrm{dx}+\mathrm{self} . \mathrm{dv} * \operatorname{self} . \mathrm{w} 0 * \mathrm{k} * \mathrm{v} \_\mathrm{p} * \mathrm{dx}+\mathrm{self} . \mathrm{dw} *\)
                self.w0 \(6 k * w \_p * d x+\) self. \(d w * k * p \_p * d x+\) self. \(d p * k * w \_p * d x\)
        B_MAT \(=\backslash\)
                self.du*u_p*dx+self.dv*v_p*dx+self.dw*w_p*dx
    \#
    \(\mathrm{Ar}=\) PETScMatrix ()
    assemble (Fp_real, tensor=Ar)
    [bc.apply (Ar) for \(b c\) in \(b c s \_p\) ]
    \(\mathrm{Ai}=\) PETScMatrix ()
    assemble (Fp_imag, tensor=Ai)
    [bc.apply (Ai) for \(b c\) in bcs_p]
        \(\mathrm{M}=\operatorname{PETScMatrix}()\)
```

        assemble (B_MAT, tensor \(=\mathrm{M}\) )
        \#【bc.apply (M) for bc in bcs_p]
        \#
        bcinds \(=\) []
        for \(b c\) in \(b c s p\) :
        bcdict \(=\) bc.get_boundary_values ()
        bcinds.extend (bcdict.keys())
        \# This just converts PETSc to CSR
        \(\mathrm{Ar}=\mathrm{sp} . \mathrm{csr}\) matrix (Ar.mat().getValuesCSR()[:: - 1\(]\) )
        \(\mathrm{Ai}=\mathrm{sp} \cdot \mathrm{csr}\) _matrix \((\mathrm{Ai} . \operatorname{mat}() \cdot \operatorname{getValuesCSR}()[::-1])\)
        \(\mathrm{M}=\mathrm{sp} \cdot \mathrm{csr}\) _matrix (M.mat(). getValuesCSR () \([::-1])\)
        \# Create shift matrix
        \#shift \(=1.2345\) e10*np.ones(len(bcinds))
        \(\# S=s p . c s r_{-}\)matrix ((shift, (bcinds, bcinds)), shape=Ar.shape)
        \(\mathrm{v}, \mathrm{V}=\operatorname{eigs}(\mathrm{Ar}+1 . j * \mathrm{Ai}, \quad 10, \mathrm{M}, \operatorname{sigma}=-1\).
        sigma[i], omega[i]=np.sort(v)[0].real, np.sort(v) [0].imag
        print ( \(\operatorname{Re}=\{ \}, \mathrm{k}=\{ \}\) lowest_sigma \(=\{ \}, \quad\) omega \(=\{ \}\), format \((\operatorname{Re}, \mathrm{ck}\),
        sigma[i],omega[i]))
    return sigma,omega
    def mymeshrefine (self):
\#REFINE CLOSE TO THE BORDER
\#TRY 3 REFINEMENTS IN THE BEGINNING
\#@30\% 15\% 5\% of the box
dist_pc=np.array ([0.1, 0.01])
distx_left $=-$ self.Gamma/2.+dist_pc*self.Gamma
distx_right $=$ self.Gamma/2.-dist_pc*self.Gamma
disty_bottom $=-1 . / 2 .+$ dist_pc*1.
disty_top $=1 . / 2 .-$ dist_pc*1
for $i$ in range(len(dist_pc)):
cell_markers = CellFunction ("bool", self.mesh)
cell_markers.set_all (False)
for cell in cells (self.mesh) :
$\mathrm{p}=$ cell.midpoint ()
if $((\mathrm{p} \cdot \mathrm{x}()<$ distx_left[i]) or
(p.x()>distx_right[i]) or
(p.y()<disty_bottom[i]) or
(p.y()>disty_top[i])):
cell_markers[cell]=True
self.mesh=refine(self.mesh, cell_markers)
def getsignchange(self, inarr):
$n \mathrm{r}=0$
change $=[]$
indices $=[]$
for $i$ in range(np.size(inarr) -1 ):
if (inarr $[i]>=0$ and inarr $[i+1]<0)$ :
$\mathrm{nr}+=1$
change. append (1)
indices.append (i)
elif (inarr $[i]<=0$ and inarr $[i+1]>0)$ :
$n \mathrm{r}+=1$
change. append (-1)
indices.append (i)
return $n r, n p$.array (change), np. array (indices)
def find_nearest(self, array, value):
array $=$ np.asarray (array)
$\operatorname{idx}=(n p . a b s(\operatorname{array}-$ value) $) \cdot \operatorname{argmin}()$
return idx, array[idx]
def plot_k_sigma(self, Re, filename):

```
    plotfile=open(filename, 'r')
    data=plotfile.readlines ()
    data_arr=np.zeros ([len(data), 2])
    for \(i\), line in enumerate(data):
        data_arr[i, 0], data_arr[i, 1] =float (line.split () [0]), float (line.split
            () [1])
    \#sort the array
    temp \(=\) np.argsort (data_arr, 0 ) \([:, 0]\)
    sorted_arr=data_arr [temp]
    \#SET MATPLOTLIB TeX
    plt.rc('font', \(* *\{\) 'family':'serif', 'serif' \(:[\) 'Times'] \(\})\)
    plt.rc('text', usetex=True)
    def cm2inch (value):
        return value/2.54
        fig, \(\mathrm{ax}=\mathrm{plt} . \operatorname{subplots}(1, \mathrm{figsize}=(\operatorname{cm} 2 \operatorname{inch}(13.8), \operatorname{cm} 2 \operatorname{inch}(7.0)))\)
        ax.plot (sorted_arr [:, 0], sorted_arr [:, 1], c='r', linestyle='-')
        ax.grid (True, which='both', \(1 \mathrm{~s}={ }^{\prime \prime}--{ }^{\prime \prime}, \mathrm{lw}=0.15\) )
        ax.set_title('Stability for \(\operatorname{Re}=\{ \}^{\prime}\). format \((\operatorname{Re})\) )
        ax.title.set_weight ('bold')
        ax.set_xlim ([0, 10.])
        ax.set_xlabel(r"k", labelpad=1.)
        ax.set_ylabel (r"\$
        savename=self.calcdir+'/'+'Re_\{:07.1f \(\}\).pdf'. format (Re)
        plt.savefig (savename, format \(=\) ' pdf , , dpi=fig.dpi)
    def readdataset (self, Gamma, angle, Re) :
    folder ='Gamma_\{:07.3f \(\}_{-}\)alpha_ \(\{: 05.1 \mathrm{f}\}\) '. format (Gamma, angle)
    filename \(=\) folder + '/' + ' \(\operatorname{Re}^{\prime}{ }^{\prime}+{ }^{\prime},\{: 08.3 \mathrm{f}\}{ }^{\prime}\) '. format (Re)
    Refile=open(filename, 'r')
    lines=Refile.readlines ()
    \(\operatorname{karr}=n \mathrm{p} . \operatorname{zeros}(\operatorname{len}(\operatorname{lines}))\)
    sigma_arr=np.zeros (len(lines))
    omega_arr=np.zeros (len(lines))
    for i , line in enumerate(lines):
        karr \([i]=\) float (line.split () [0])
        sigma_arr \([i]=\) float (line.split () [1])
        omega_arr[i] \(=\) float (line.split () [2])
    return karr, sigma_arr,omega_arr
def get_kneutral(self, Gamma, alpha, Re):
    karr, sigma_arr,omega_arr=self.readdataset (Gamma, alpha, Re)
    nr, changearr, indices=self.getsignchange (sigma_arr)
    if \((\mathrm{nr}=0)\) :
        return 0
    else:
            return karr[indices], sigma_arr[indices], omega_arr[indices]
\#A FUNCTION WHERE WE COMPARE DIFFERENT CURVES
\#plotarr has to be a dictionairy that provides the Gamma, Re, angle values
        def compareplot(self, plotarr, show=True):
            \#SET MATPLOTLIB TeX
            plt.rc('font', \(* *\{\) 'family','serif', 'serif': ['Times'] \(\}\) )
            plt.rc('text', usetex=True)
            def cm2inch (value) :
            return value \(/ 2.54\)
        fig, \(\mathrm{ax}=\mathrm{plt} . \operatorname{subplots}(1, \mathrm{figsize}=(\operatorname{cm} 2 \operatorname{inch}(13.8), \operatorname{cm} 2 \operatorname{inch}(7.0)))\)
        ax.grid (True, which='both ', \(1 \mathrm{~s}==^{\prime \prime}-\) ' \(^{\prime}, \mathrm{lw}=0.15\) )

                '\#009999']
```

    for i in range(len(plotarr)):
        Gamma=plotarr[i][ 'Gamma']
        Re= plotarr[i]['Re']
        angle = plotarr[i]['angle']
        label = r'$\alpha={:5.2f} \Gamma={:5.2f} Re={:8.2f}$'.format(angle,
                Gamma,Re)
        karr,sigma_arr,omega_arr=self.readdataset(Gamma, angle,Re)
        #SORT THE ARRAYS
        sigma_arr=sigma_arr[np.argsort(karr)]
        omega_arr=omega_arr[np.argsort (karr)]
        karr = np.sort(karr)
        ax.plot(karr,sigma_arr, c=colors[i], linestyle='-', label=label)
        ax.set_xlabel(r"k", labelpad=1.)
        ax.set_ylabel(r"$\sigma$", labelpad=1.)
        ax.legend()
        if(show):
        plt.show()
        else:
        plt.savefig('TEMPPLOT.pdf', format='pdf', dpi=fig.dpi)
    def analyze_k_n(self,Re,relax_param,k1,k2,ngrid):
    print('RUNNING ANALYZE_K WITH REYNOLDS: {} \n k1 = {} k2 = {}'.format(
        Re,k1,k2))
    filename=self.calcdir+'/'+'Re_k'+'_{:08.3 f }'.format(Re)
    Refile=open(filename, 'w')
    karr=np.linspace(k1,k2,3)
    nx=ngrid
    ny=ngrid
    self.getbaseflow(Re, nx, ny, relax_param)
    sigma,omega=self.linearstab(Re, karr)
    for line in range(len(sigma)):
        Refile.write('{:10g} {:10g} {:10g} \n'.format(karr[line],
                sigma[line],omega[line]))
    nr, changearr, indices=self.getsignchange(sigma)
    Refile.close()
    def gamma_angle_Re(gammaarr, anglearr, Rearr,relax_param_arr):
for Gamma in gammaarr:
for angle in anglearr:
print(,',
%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%
CALCULATING GAMMA ={:07.3 f } AND ANGLE ={:05.1 f}
%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%, , ', format (Gamma, angle )
)
folder='Gamma_{:07.3f}_alpha_{:05.1f }'.format(Gamma, angle )
cav=mycav(Gamma, angle, calcdir=folder)
for Re,relax_param in zip(Rearr, relax_param_arr):
cav.analyze(Re,relax_param)
def RcAnalysis(gammaarr, anglearr):
for Gamma in gammaarr:
for angle in anglearr:
print(,,,
%%%%%%%%%%%%%%%%%%%%0%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%
ReC analysis: GAMMA ={:07.3f} AND ANGLE ={:05.1f}
%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%, , ', format (Gamma, angle )
)
folder='Gamma_{:07.3f}_alpha_{:05.1f}'.format(Gamma, angle)
cav=mycav(Gamma, angle, calcdir=folder)

```
```

    Re_low=300
    Re_high=900
    cav.findRe_c(Re_low, Re_high)
    \#TODO: WRITE A FUNCTION TO SAVE THE VELOCITY-FIELD
if __name__='__main__ ':
\#Gammaarr=np.array ([1., 0.5, 2., 3.])
\#anglearr=np.array([0.,22.5,45,67.5])
\#Rearr = [700,750,800,850,900,950,1000]
\#Rearr2 = [710,720,730,740,760,770,780,790,810,820,830,840]
\#\#gamma_angle_Re(Gammaarr, anglearr, Rearr2)
RcAnalysis(Gammaarr, anglearr)

```

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[^0]:    ${ }^{1}$ Feynman R. 1964.

[^1]:    ${ }^{1}$ This derivation follows the introduction to fluid dynamics of the scriptum "Strömungslehre für TPh" by Prof. Braun (Braun (2001))

[^2]:    ${ }^{2}$ An incompressible fluid is defined as having no materials derivative of the volume, which is proportional to the divergence of $\vec{v}$ as derived in equation (A.6) in Appendix A

[^3]:    ${ }^{3}$ These definitions are taken from www.wikipedia.org

[^4]:    ${ }^{4}$ This derivation of the Reynolds-Orr equation follows the treatment in Kuhlmann (2012).

[^5]:    ${ }^{5}$ This Figure is taken from Kuhlmann (2012)

[^6]:    ${ }^{6}$ The treatment of this section follows the script "Grundlagen der numerischen Methoden der Strömungs- und Wärmetechnik" (Kuhlmann 2010)
    ${ }^{7}$ For completeness, the function space would in general have to be infinite $N \rightarrow \infty$, so completeness will only be fulfilled approximately and the convergence with respect to the number of test functions will always have to be tested.
    ${ }^{8}$ The choice of Ansatz function is crucial and should correspond to the given problem since a proper set of Ansatz functions reduces the number of necessary coefficients drastically, e.g. in quantum mechanical problems, the hydrogen orbitals are proper basis functions whereas in periodic systems plane waves are common Ansatz functions.

[^7]:    ${ }^{9} \Delta x$ denotes the grid spacing

[^8]:    ${ }^{1}$ this will be the case for all finite element calculations, unless mentioned otherwise

[^9]:    ${ }^{2}$ This thesis is mainly computed on a laptop, so the available RAM is low.
    ${ }^{3}$ Childs et al. 2012.

[^10]:    ${ }^{4}$ The vorticity $\vec{\omega}$ is given by the curl of the flow velocity: $\vec{\omega}=\vec{\nabla} \times \vec{u}$. It is a measure for the local rotation of a fluid.

[^11]:    ${ }^{2}$ The preliminary three-dimensional simulations were performed for an increased Reynolds number than the predicted critical one to assure the appearance of the instability. The simulations. For $R e=750$ and $k=7.24$ the three-dimensional simulation gives $\omega=586.8 \pm$ 8.2, which is reproduced by our calculation for this setting, yielding $\omega=579.18$.

[^12]:    ${ }^{1}$ This derivatoin also follows the treatment given in (Braun 2001)

